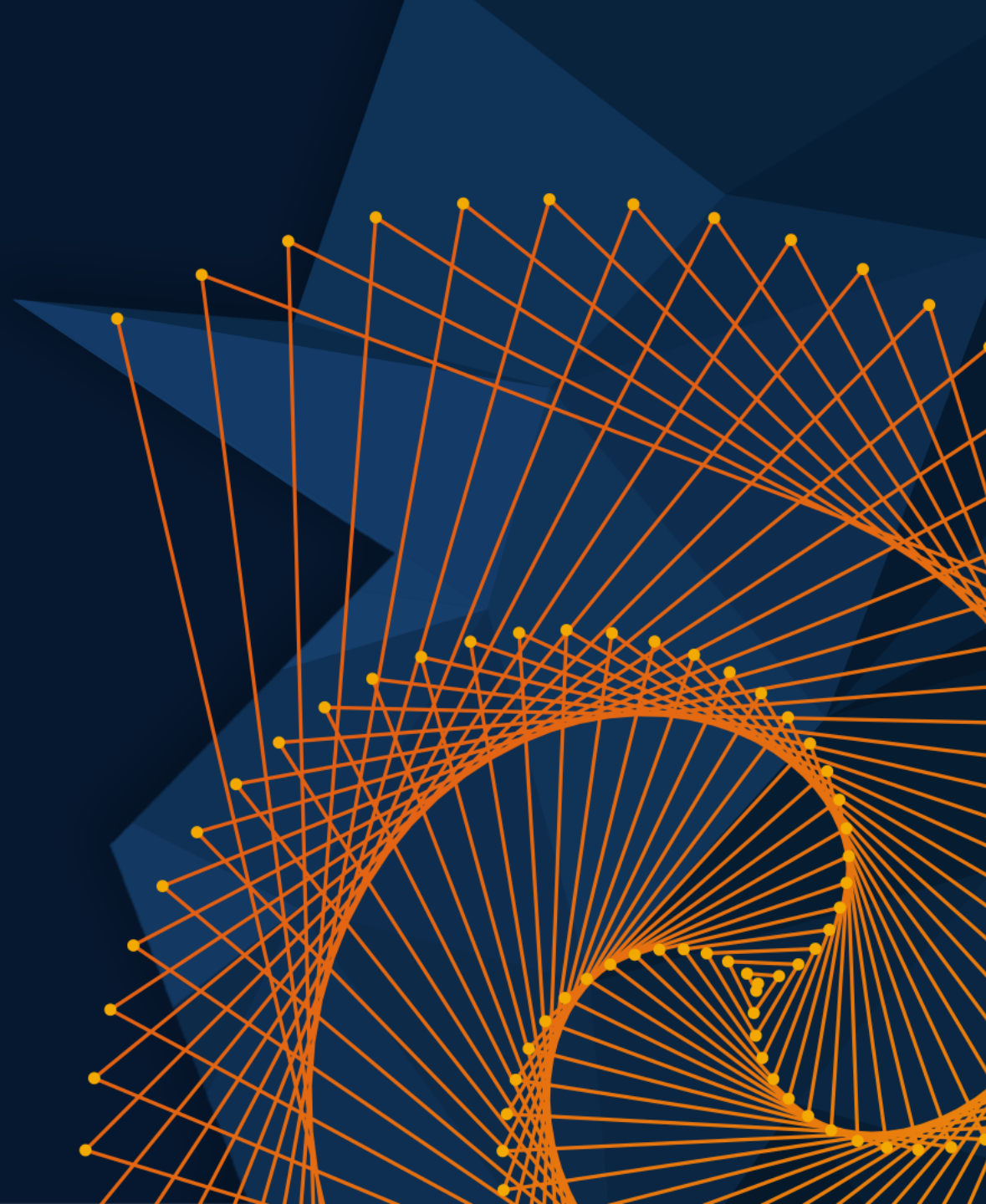


MATLAB EXPO

2024.06.11 | 그랜드 인터컨티넨탈 서울 파르나스

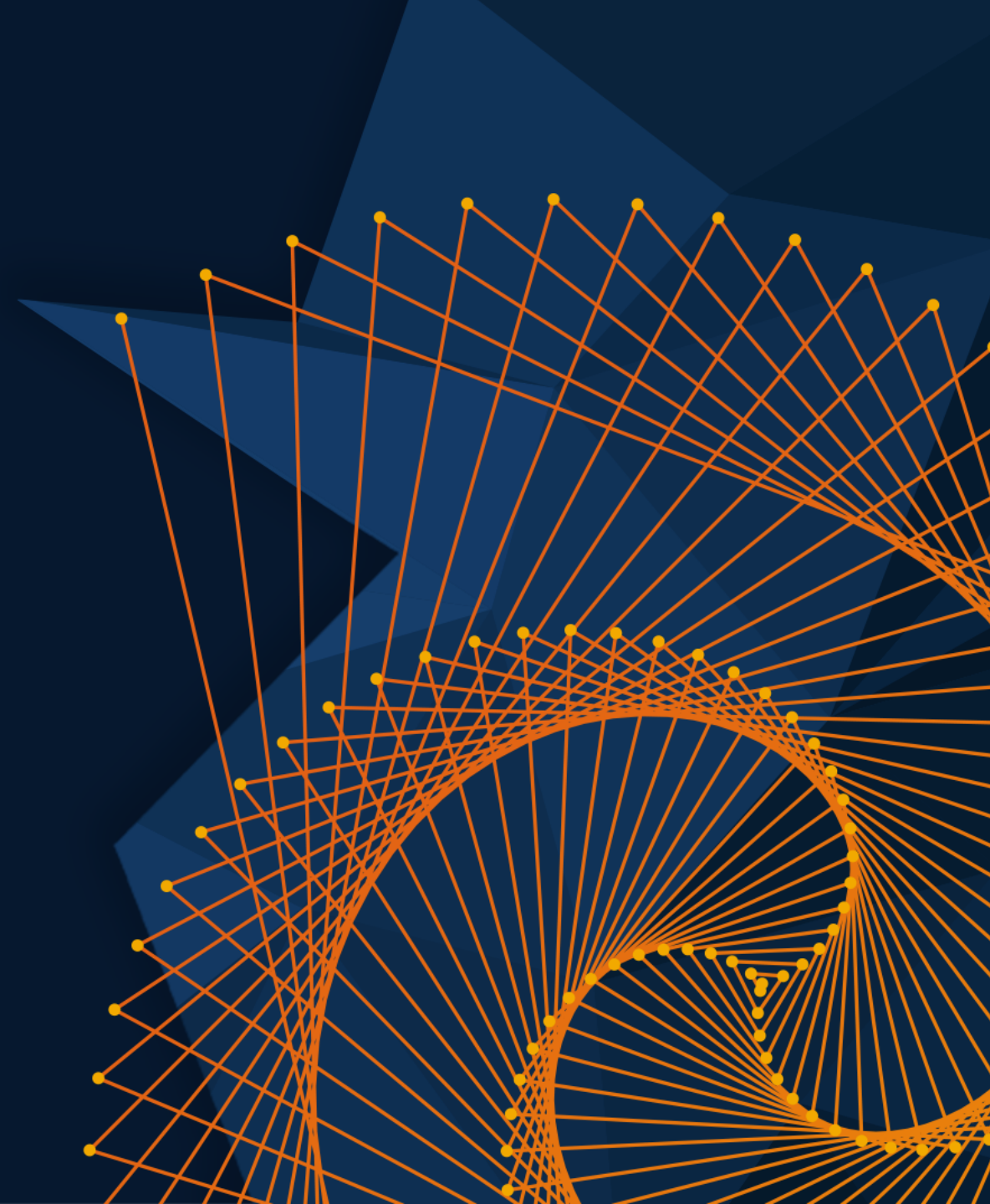
Simscape를 이용한 차량 열관리 버추얼 플랜트 개발 및 활용

김재웅 글로벌R&D마스터, 현대자동차



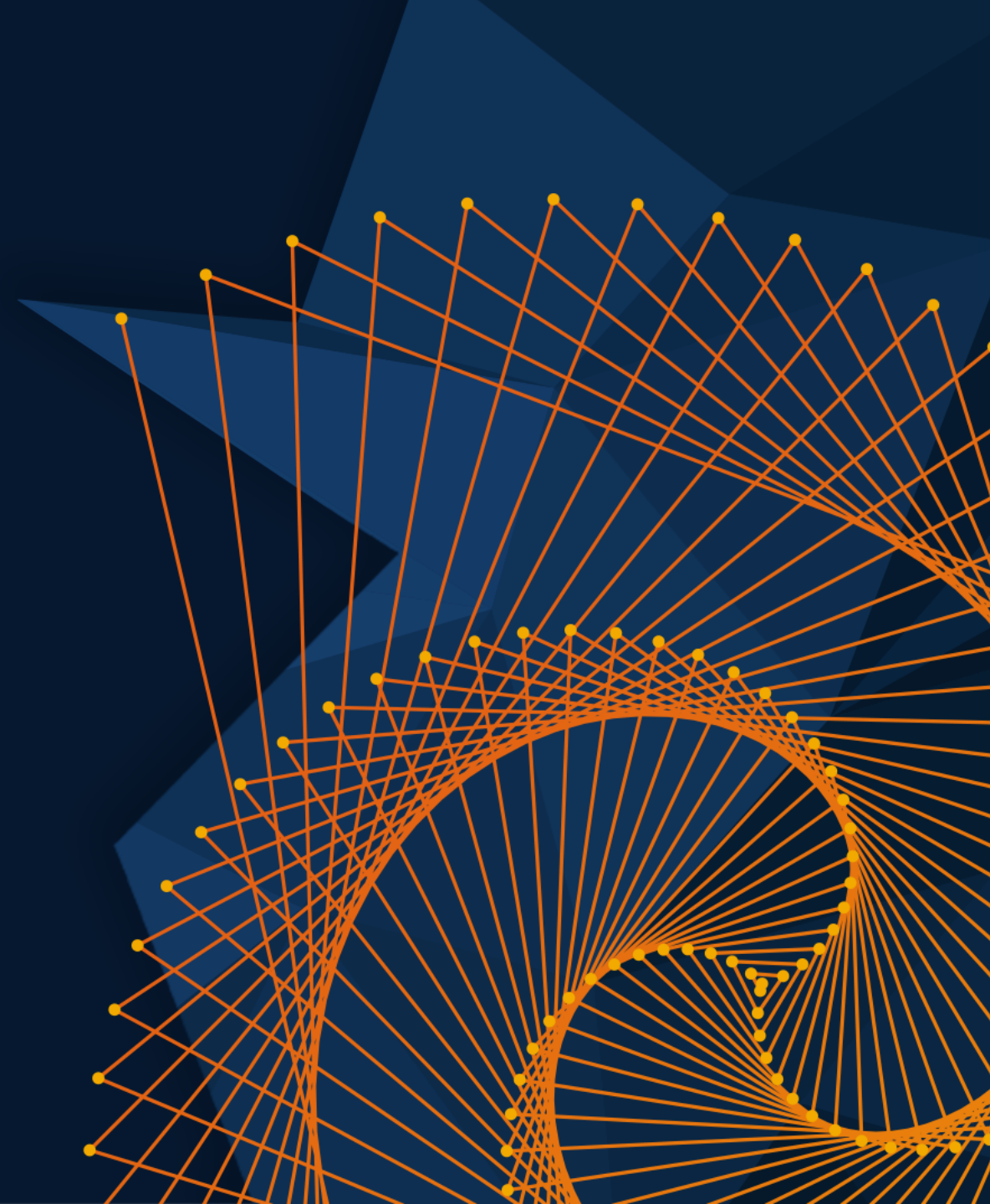
Contents

1. Introduction
2. Component level
3. System level
4. Control logic & Verification
5. Conclusion



Contents

1. Introduction
2. Component level
3. System level
4. Control logic & Verification
5. Conclusion

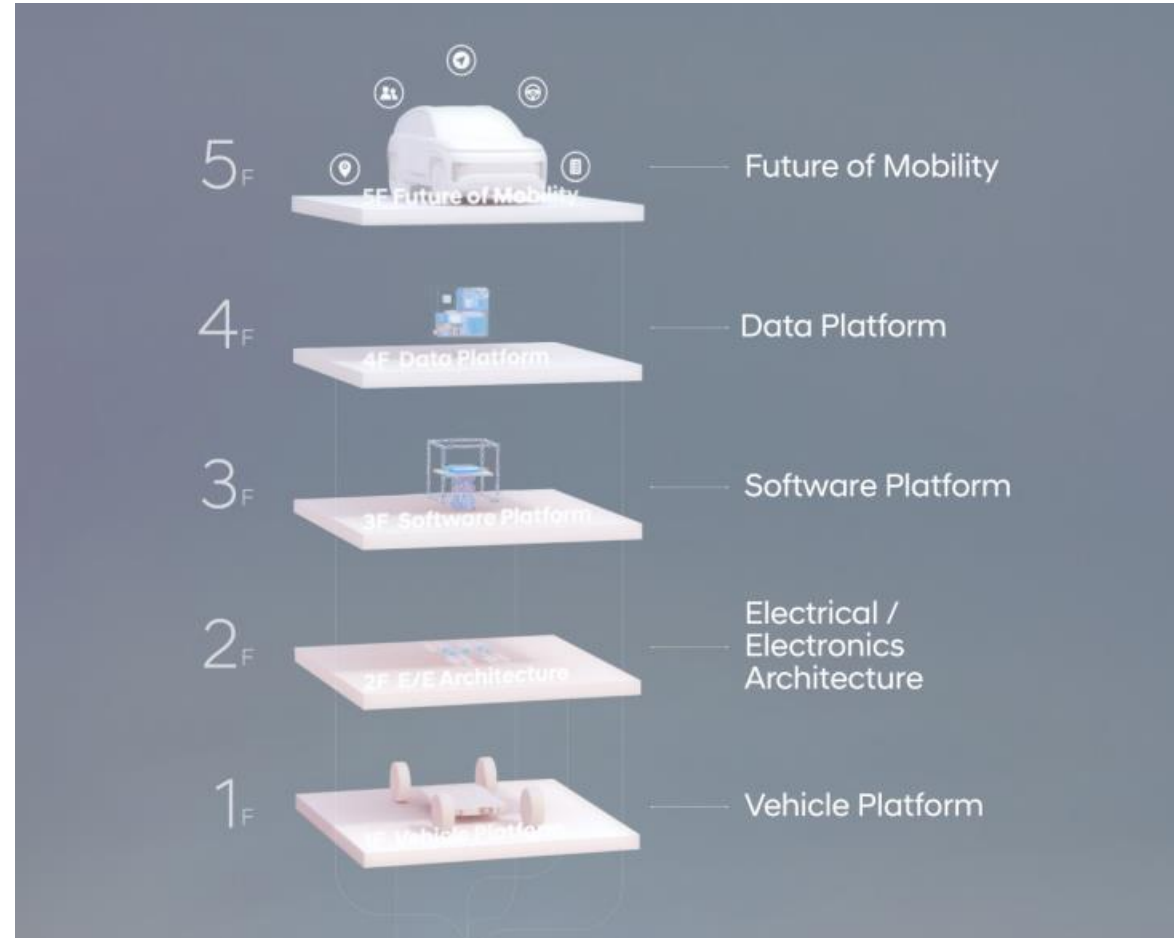


1. Introduction

- SDV



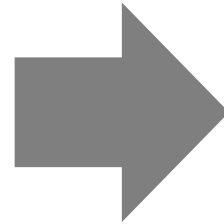
Software-defined Vehicle refers to a car where software primarily determines the functions and performance of the vehicle.



<https://www.hyundai.co.kr/live/unlock-the-software-age>

1. Introduction

- SDV : Software-defined Vehicle for new value



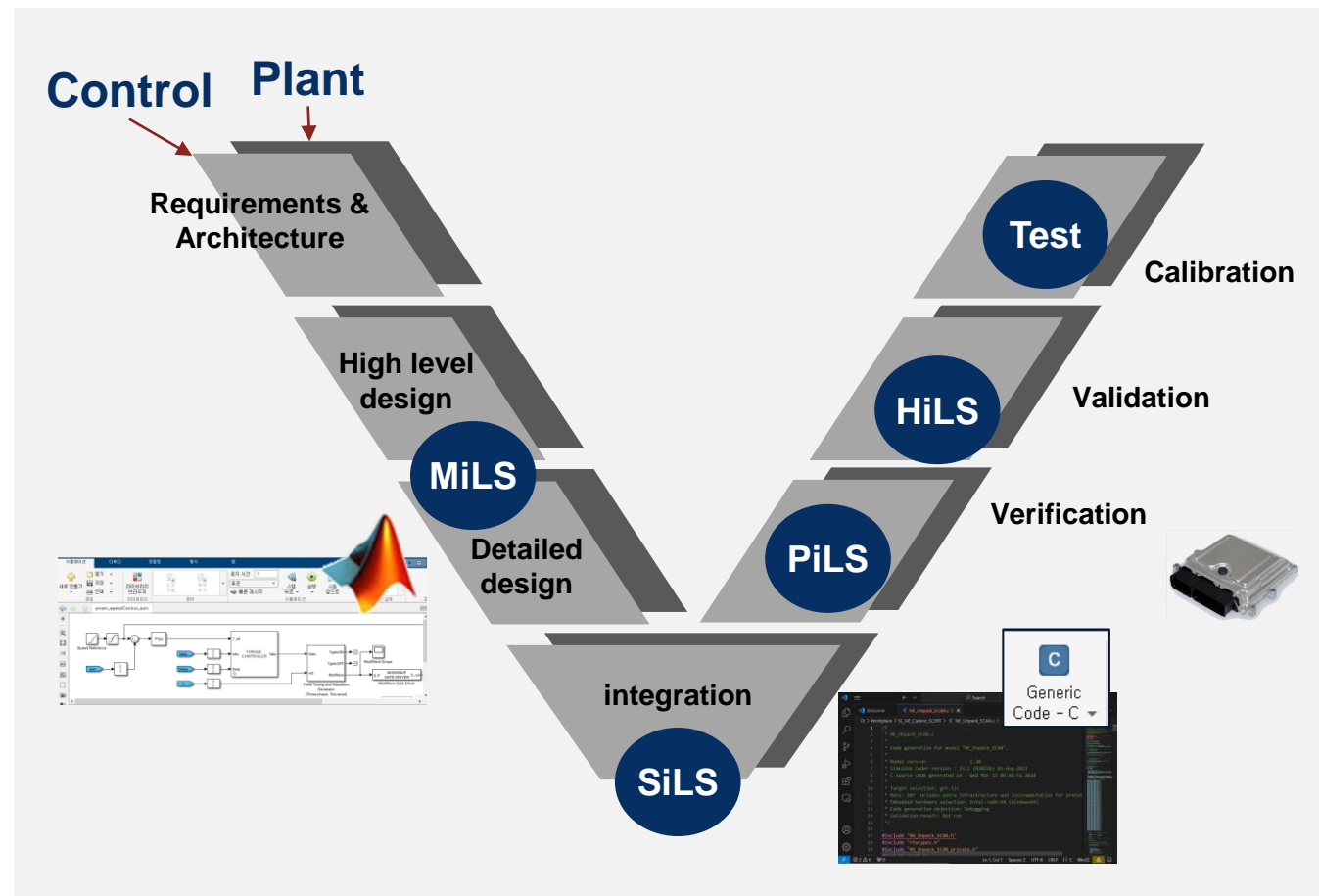
1. Introduction

- Model-based Development



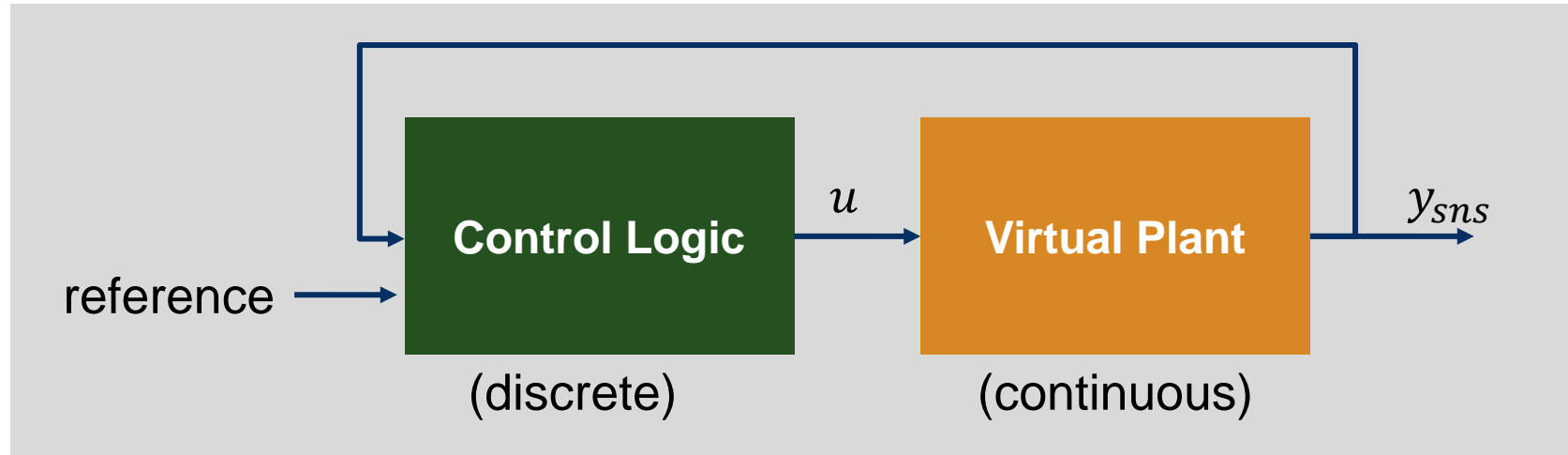
Model-based Development
for better performance and service

→ **Optimization**



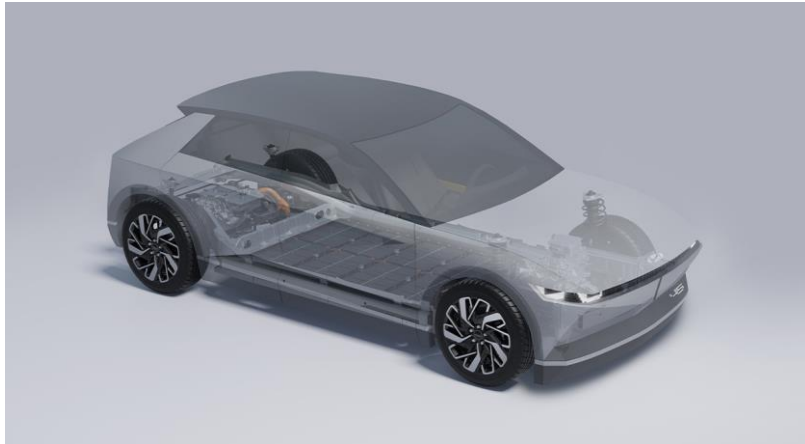
1. Introduction

- Control logic & virtual plant

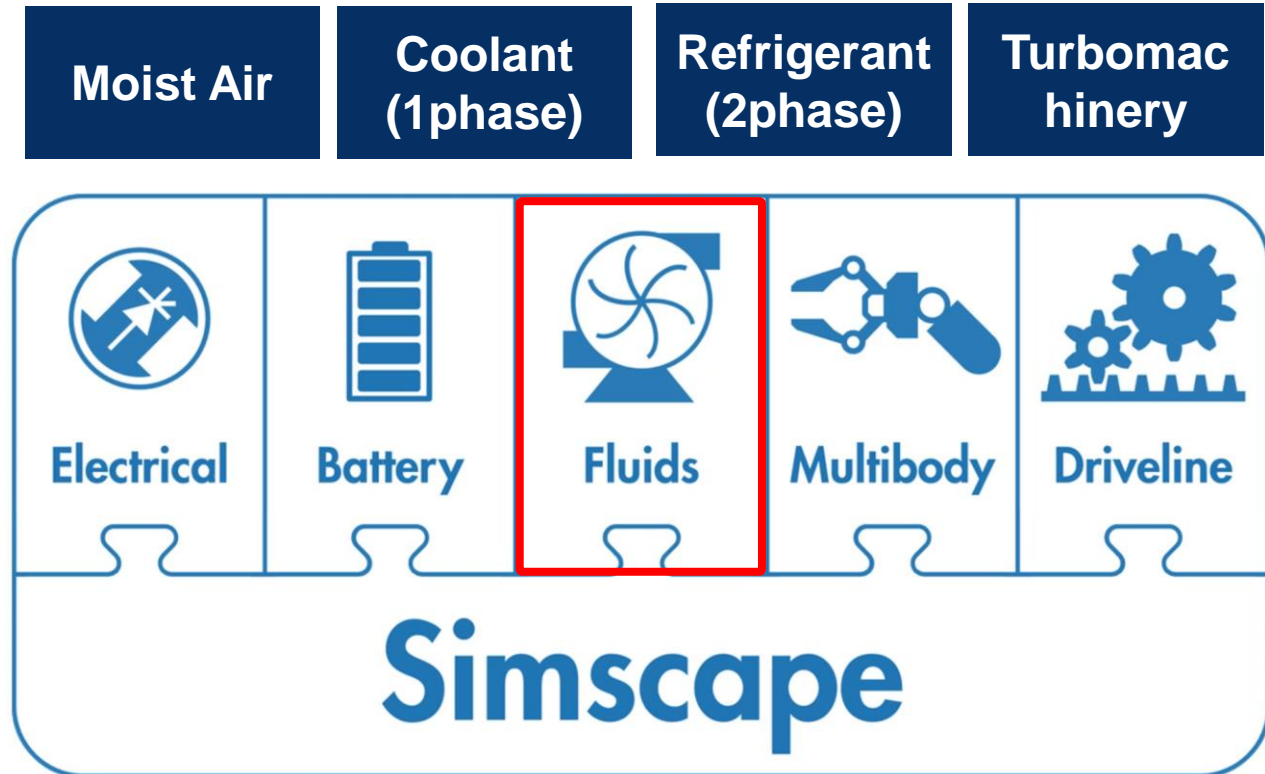


1. Introduction

- Simscape

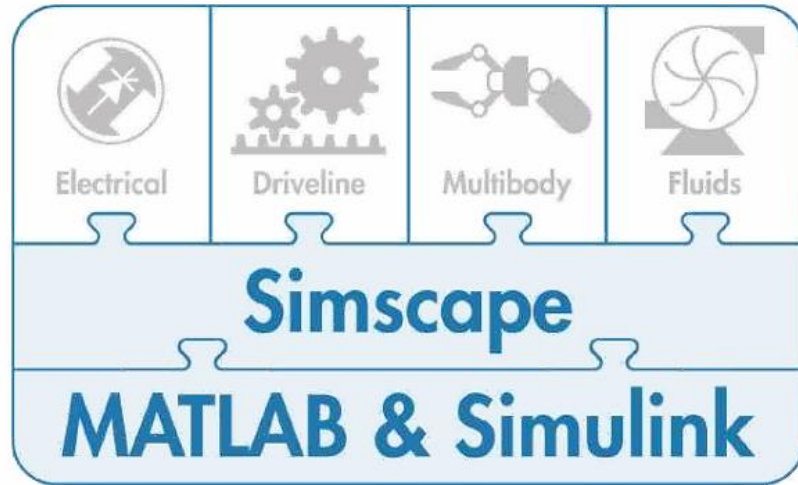


Simscape is an equation-based modeling tool for physical systems.



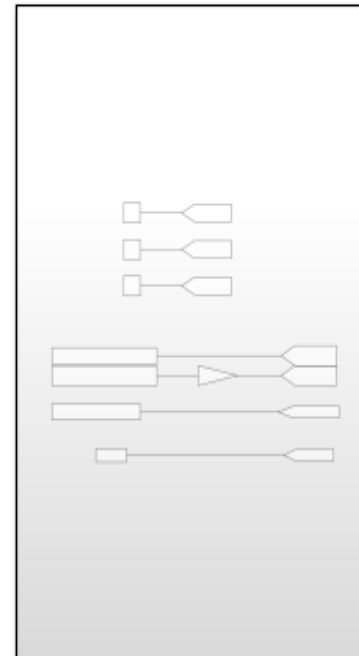
1. Introduction

- topic

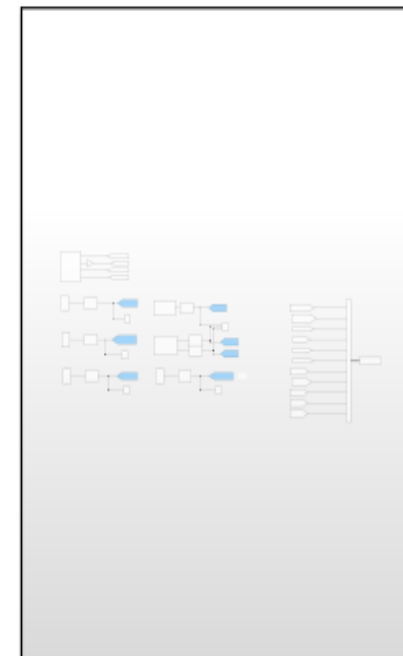


Thermal circuit
- Cooling
- Air conditioning

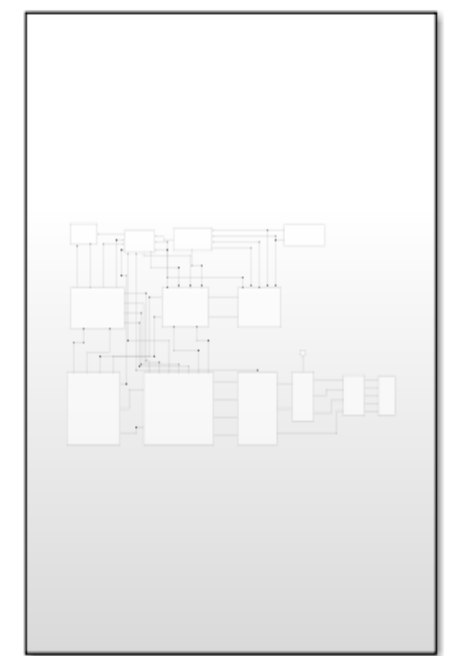
Simulink & Simscape



Environment



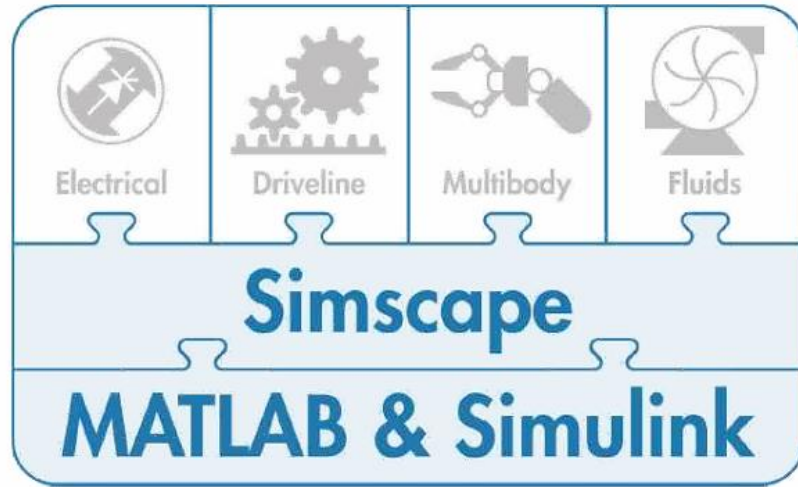
Controller



Plant

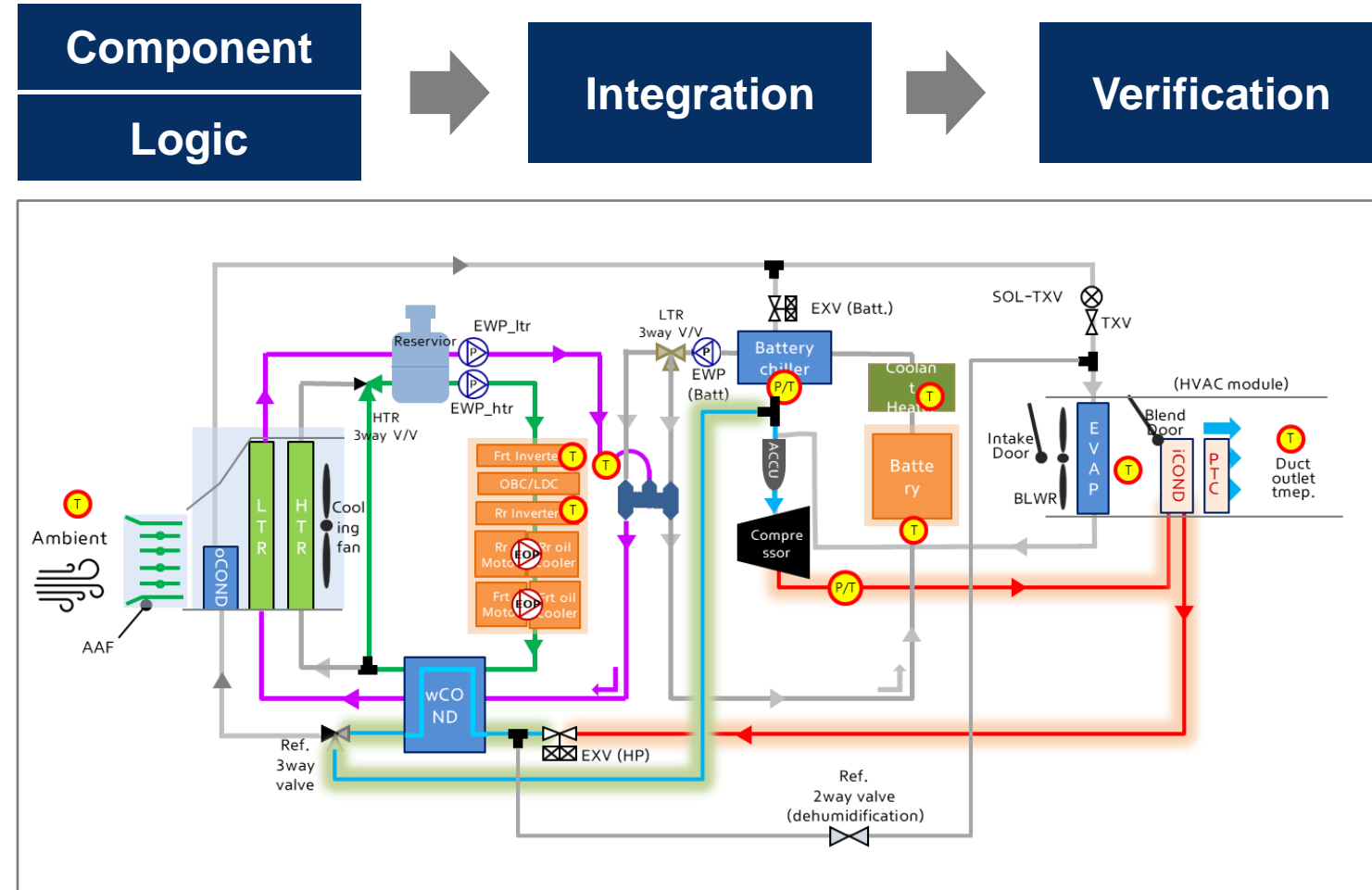
1. Introduction

- topic



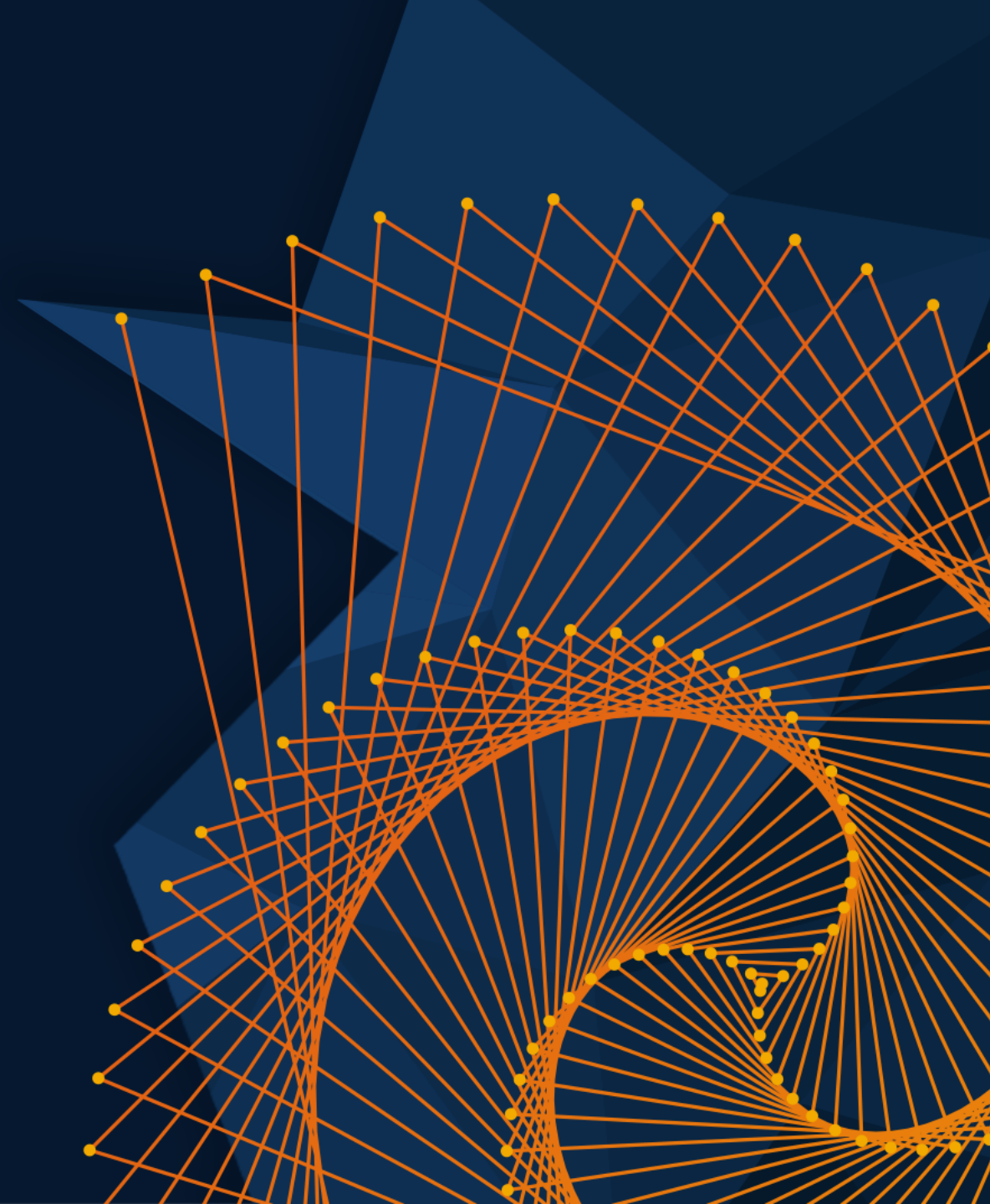
Thermal circuit

- Cooling
- Air conditioning



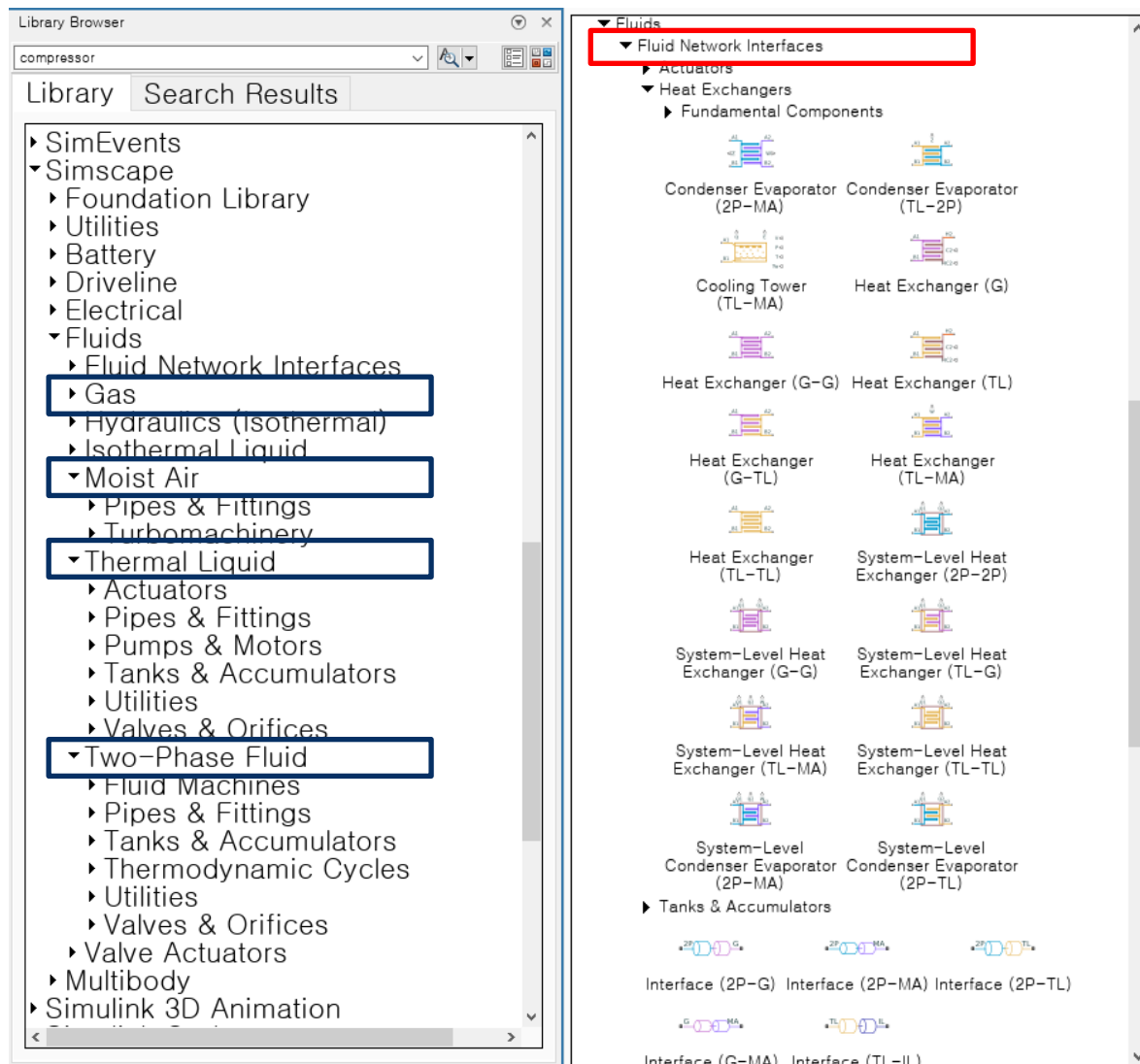
Contents

1. Introduction
- 2. Component level**
3. System level
4. Control logic & Verification
5. Conclusion



2. Component Level

- Simscape/Fluids library



G

Gas

MA

Moist Air

TL

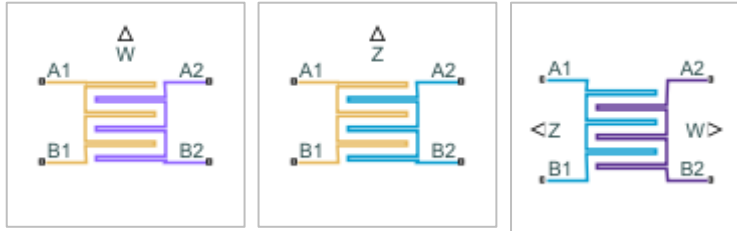
Thermal Liquid

2P

2Phase

2. Component Level - how to build the HEX

Component



Heat Exchanger : TL-MA, TL-2P, 2P-MA



Geometry info. : Length, Area, ...

필요 정보	단위	설명	COND_NE_Pilot
COND.Name	String	모듈 이름, 임의값	COND_Air_NE
COND.K	W/mK	conductivity (alum_300)	160
COND.Size.Width	m		0.61
COND.Size.Height	m		0.1266
COND.Size.Depth	m		0.016
COND.TubesInAirFlowDirection	ea	공기방향 열수	1
COND.PassNum	ea	냉매방향 열수	2
COND.TubesPerPass	ea	냉매패스 튜브수	(8 7)
COND.TubesInChannel	ea	류프당 채널수	18
COND.Tube.Thickness	m		2.50E-04
COND.Tube.Height	m		1.40E-03
COND.Fin.FPDM	ea/dm	Fin Pitch per Decimeter (상 - 굵)	80
COND.Fin.Thickness	m		7.00E-05
COND.Fin.height	m		5.60E-03
COND.Louver.angle_deg	deg		33
COND.Louver.Pitch	m		8.00E-04
COND.Louver.Height	m		5.90E-03

블록 파라미터: Condenser Evaporator (2P-MA)

Condenser Evaporator (2P-MA) 자동 적용

이름: 값

▼ Configuration

- Flow arrangement: Cross flow
- Cross flow arrangement: Both fluids unmixed
- Thermal resistance through heat tra...: 0 K/kW
- Cross-sectional area at port A1: $\pi * \text{geo.EVAP_Air.D_inlet}...$ mm²
- Cross-sectional area at port B1: $\pi * \text{geo.EVAP_Air.D_outl}...$ mm²
- Cross-sectional area at port A2: $\text{geo.EVAP_Air.Width} * \text{ge}...$ m²
- Cross-sectional area at port B2: $\text{geo.EVAP_Air.Width} * \text{ge}...$ m²

▼ Two-Phase Fluid 1

- Number of tubes: $\text{geo.EVAP_Air.nTubesPerRowPerCol}_ * \text{geo.EVAP_}...$
- Total length of each tube: $\text{geo.EVAP_Air.Width} * \text{ge}...$ m
- Tube cross section: Rectangular
- Tube width: $\text{geo.EVAP_Air.Depth} / \text{ge}...$ m
- Tube height: $\text{geo.EVAP_Air.TubeHeigh}...$ m
- Pressure loss model: Correlation for flow inside tubes
- Local resistance specification: Local loss coefficient
- Total local loss coefficient: 1000*1.2 1200
- Internal surface absolute roughness: 0.001 mm
- Laminar flow upper Reynolds numb...: 2000

▼ Moist Air 2

- Total fin surface area: $\text{geo.EVAP.Fin.AreaTotal}$ m²

2. Component Level

- how to build the HEX

Component

- Pressure loss coefficients model : $K = \frac{\Delta P}{0.5\rho v^2}$
- Heat transfer coefficients model : Colburn equation
(the measured data is available and empirical correlations usually fit better)
 - Colburn eq. For liquid and vapor zones : $Nu = aRe^b Pr^c$
 - Cavallini-Zecchin correlation for mixture zone :

Pressure loss model	Pressure loss coefficient
> Pressure loss coefficient, delta_p/(0...	350
Heat transfer coefficient model	Colburn equation
> Coefficients [a, b, c] for a*Re^b*Pr...	[iCond_ref_a1, .8, .33]
> Coefficients [a, b, c] for a*Re^b*Pr...	[iCond_ref_a2, .8, .33]
> Coefficients [a, b, c] for a*Re^b*Pr...	[iCond_ref_a3, .8, .33]

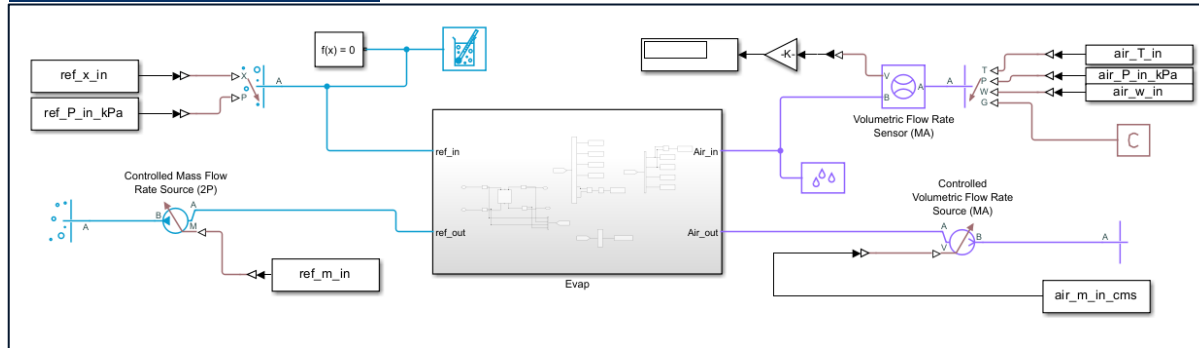
$$h = Nu \frac{k}{D}$$

$$Nu = \frac{aRe_{SL}^b Pr_{SL}^c \left\{ \left[\left(\sqrt{\frac{\rho_{SL}}{\rho_{SV}}} - 1 \right) x_{Out} + 1 \right]^{1+b} - \left[\left(\sqrt{\frac{\rho_{SL}}{\rho_{SV}}} - 1 \right) x_{In} + 1 \right]^{1+b} \right\}}{(1+b) \left(\sqrt{\frac{\rho_{SL}}{\rho_{SV}}} - 1 \right) (x_{Out} - x_{In})}$$

2. Component Level

- how to build the HEX

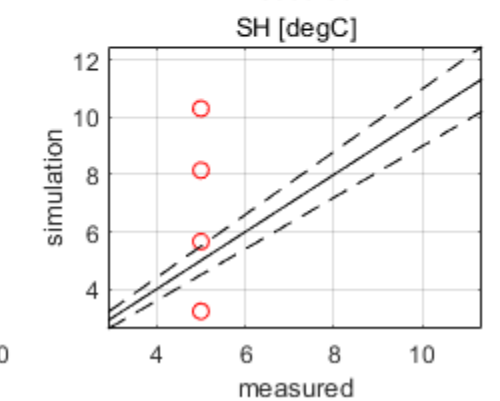
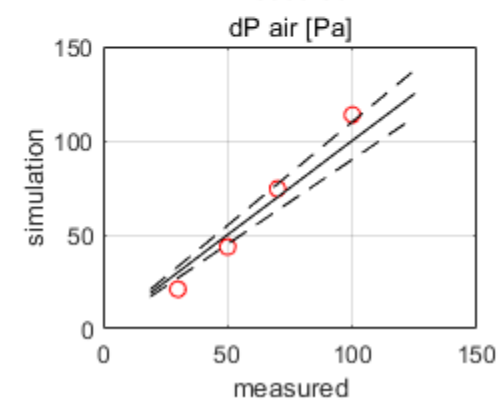
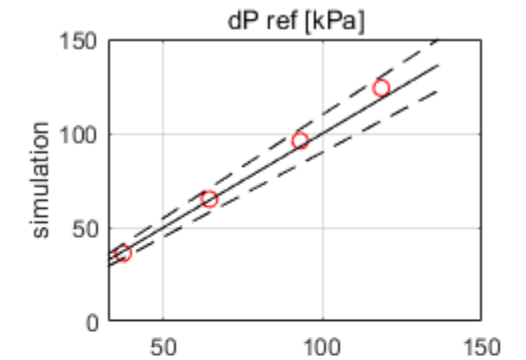
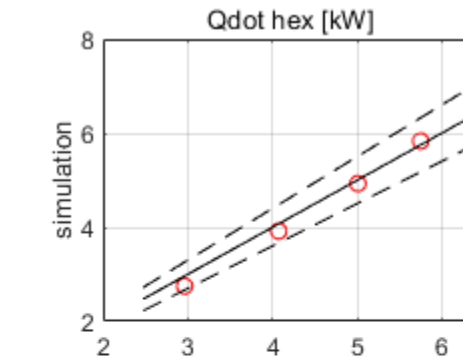
Unit bench



- ① Pressure drop
 - ② Heat transfer, Temperature,...
- ↑
- System Identification
(Optimization tool)
→ parameter tuning

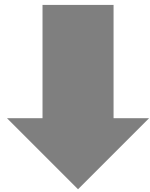
Performance sheet

Time	Air Velocity (m/s)		$T_{air_out}(^{\circ}C)$	$dP_{air}(Pa)$	$Q_{air}(kW)$	$Q_{refrige\ rant}(kW)$	냉매유량 (kg/h)	$T_{ref_in}(^{\circ}C)$	$T_{ref_out}(^{\circ}C)$	Pref_in(kPa(gauge))	Pref_out(kPa(gauge))	Subcool ($^{\circ}C$)		
0	2.0	37.0	0.041	54.40	0.011	41.7	3.3	3.3	77	85.5	54.90	1560.6	1541.0	5.0
200	3.0	37.0	0.041	52.80	0.011	75.3	4.5	4.5	108	85.5	54.40	1560.6	1526.4	5.0
400	4.0	37.0	0.041	51.60	0.011	115.8	5.4	5.4	128	85.5	54.50	1560.6	1508.0	5.0
600	5.0	37.0	0.041	49.90	0.011	163.7	6.0	6.0	139	85.5	54.40	1560.6	1494.0	5.0



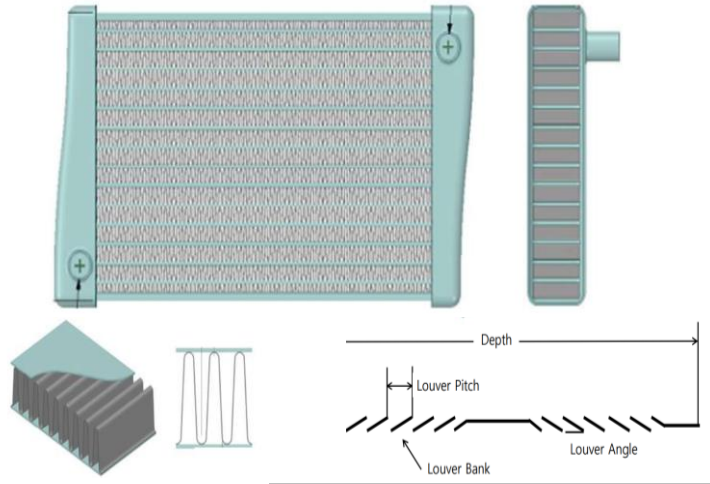
2. Component Level - Heat Exchanger (TL-MA)

Geometry
performance

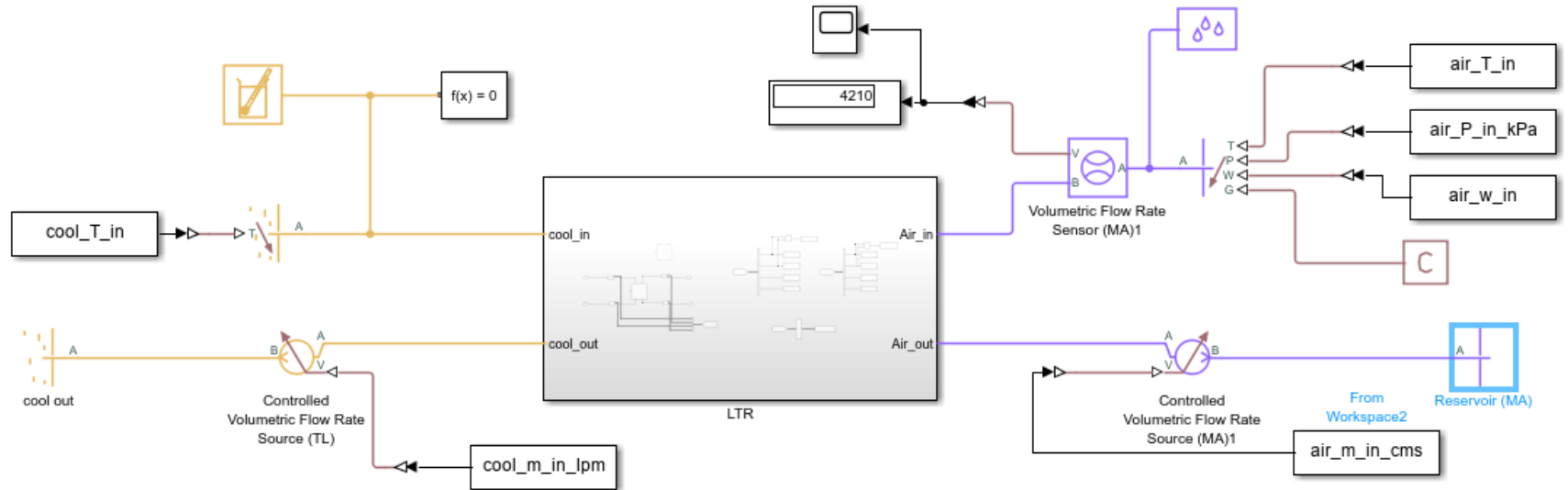


Modeling

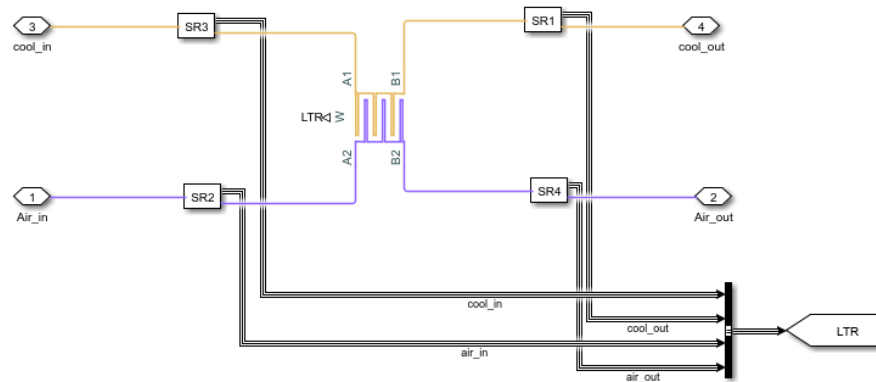
- Geometry info.
- Pressure loss
- Heat transfer



Input					Output		
Time	Vair [m/s]	Tair_in [degC]	Tcool_in [degC]	Qm_cool [lpm]	Q_dot_hex [W]	dP_air [Pa]	dP_cool [Pa]
Time	vair_mps	Tair_in	Tcool_in	LPM	Q_dot	dP_air_Pa	dP_cool_Pa
0	2	20	40	8	4.665	25.195	10.623
50	4	20	40	8	5.800	42.529	17.35.6
100	5	20	40	8	6.309	100.402	17.833.4
150	6	20	40	8	6.557	255.995	18.248.7
200	7	20	40	10	6.804	25.396	20.810.0
250	8	20	40	10	6.864	69.438	21.555.3
300	8	20	40	10	7.079	160.503	22.497.2
350	8	20	40	12	7.393	257.169	23.688.4
400	8	20	40	12	6.917	25.377	25.599.8
450	8	20	40	12	8.992	82.327	28.207.4
500	8	20	40	12	7.636	100.604	27.923.7
550	8	20	40	12	8.090	257.970	28.357.8



2. Component Level - Heat Exchanger (TL-MA)



NAME	VALUE
Configuration	
Flow arrangement	Cross flow
Cross flow arrangement	Both fluids unmixed
Thermal resistance through heat tra...	0 K/KW
Cross-sectional area at port A1	$\pi * \text{geo.LTR.D_inlet}^2 / 4$ mm ²
Cross-sectional area at port B1	$\pi * \text{geo.LTR.D_outlet}^2$ mm ²
Cross-sectional area at port A2	$\text{geo.LTR.Width} * \text{geo.LTR.}$ m ²
Cross-sectional area at port B2	$\text{geo.HTR.Width} * \text{geo.HT.}$ m ²
Thermal Liquid 1	
Flow geometry	Flow inside one or more tubes
Number of tubes	$\text{geo.LTR.nTubesPerRowPerCol}$ 29
Total length of each tube	$\text{geo.LTR.Width} * \text{geo.LTR.}$ m
Tube cross section	Rectangular
Tube width	$\text{geo.LTR.Depth} - \text{geo.LT.}$ m
Tube height	$\text{geo.LTR.TubeHeight-geo.}$ m
Pressure loss model	Pressure loss coefficient
Pressure loss coefficient, delta_p/(0...	1.09
Heat transfer coefficient model	Colburn equation
Coefficients [a, b, c] for a*Re ^b Pr ^c	[LTR_cool_a, 8, 33] [0.012, 0.8033]
Fouling factor	0 K ² m ² /KW
Total fin surface area	0 m ²
Fin efficiency	1
Initial thermal liquid pressure	Ambient_P 101.31 kPa
Initial thermal liquid temperature	Ambient_T 20 degC
Moist Air 2	
Flow geometry	Generic
Minimum free-flow area	$\text{geo.LTR.Width} * \text{geo.LTR.}$ m ²
Heat transfer surface area without fi...	$\text{geo.LTR.nTubesPerRowP.}$ m ²

$$dP = K \left(\frac{1}{2} \rho V^2 \right)$$

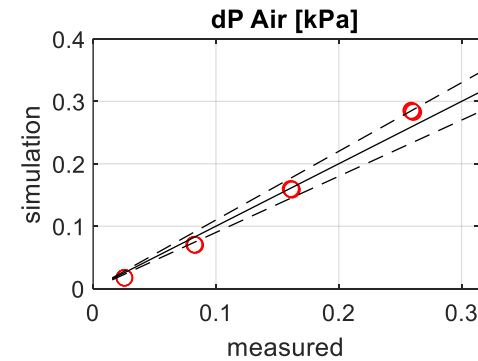
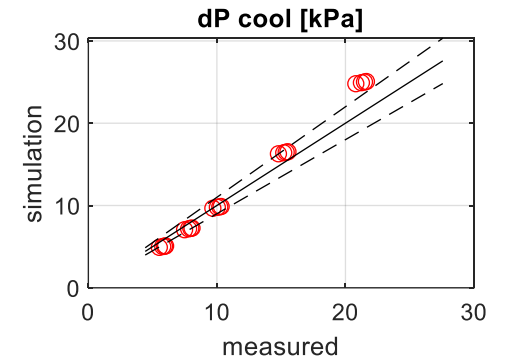
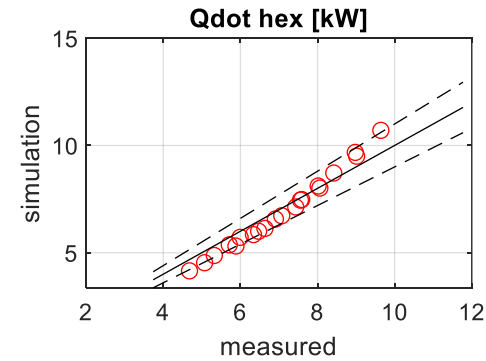
(pressure loss coefficient)

$$h = Nu \frac{k}{D}$$

$$Nu = a Re^b Pr^c$$

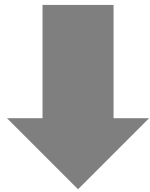
(Colburn equation)

Pressure drop → Heat transfer



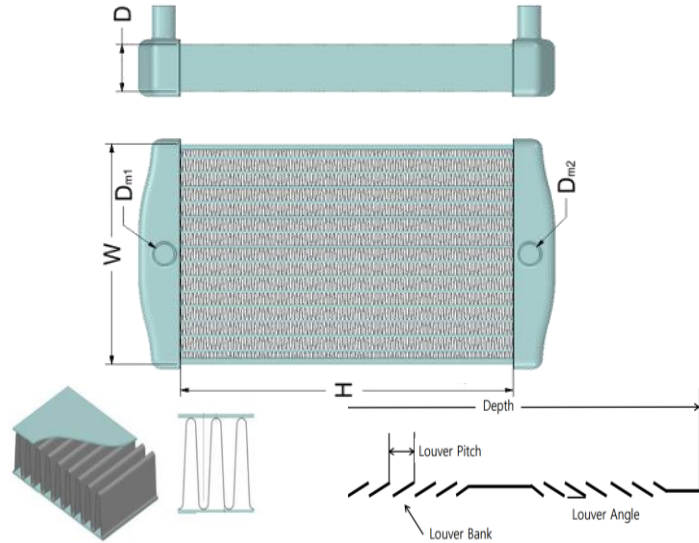
2. Component Level - Heat Exchanger (2P-MA)

Geometry
performance

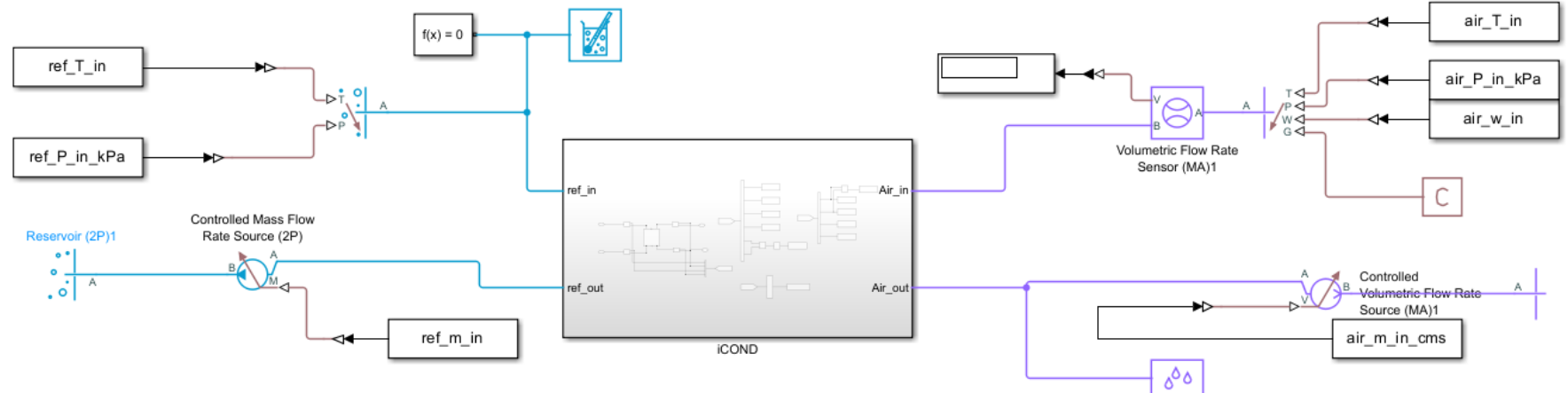


Modeling

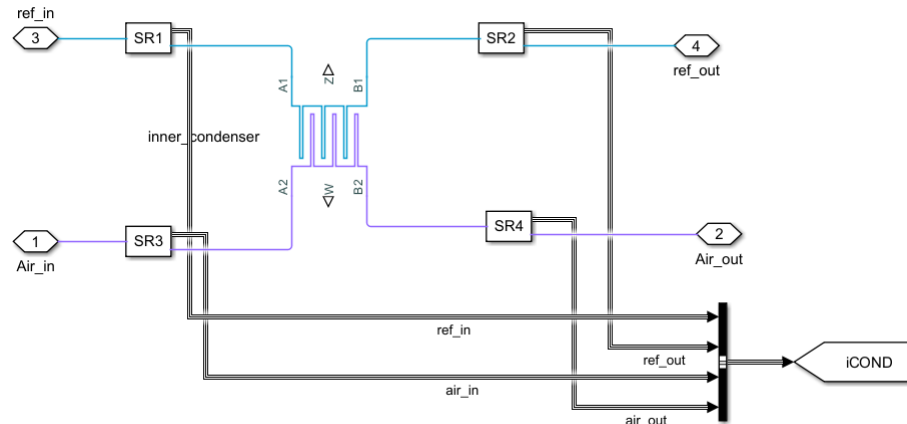
- Geometry info.
- Pressure loss
- Heat transfer



Time	Air side										Refrigerant side				
	CMFS	Tair_in	ref_in_abs	Tair_out	ref_out_abs	dP_airPa	Q_airkW	Q_refrigerant	ref_ref_kgPa	Tref_in	Tref_out	ref_in_kPa_gauge	ref_out_kPa_gauge	ref_ref	
0	0.0000	15	0.004	59.0	0.004	112.5	0.00	0.00	0.0355	100	64.78	2.257.00	2.251.18	11.00	
100	0.0000	15	0.004	61.1	0.004	101.2	5.44	5.44	0.0319	100	64.8	2.257.00	2.252.03	11.00	
200	0.0000	15	0.004	62.3	0.004	86.9	4.79	4.79	0.0281	100	64.8	2.257.00	2.252.93	11.00	
300	0.0000	15	0.004	58.5	0.004	62.2	4.09	4.09	0.024	100	64.83	2.257.00	2.253.73	11.00	
400	0.0000	15	0.004	64.6	0.004	47.7	3.34	3.34	0.0196	100	64.84	2.257.00	2.254.53	11.00	
500	0.07	15.09	0.004	62.96	0.004	48.06	2.73	3.97	0.02816325	102.00	67.46	2.263.54	2.256.65	9.98	
600	0.10	15.00	0.004	61.14	0.004	76.60	5.11	5.21	0.03687138	102.00	67.40	2.266.56	2.256.48	9.95	
700	0.13	14.96	0.004	78.11	0.004	111.21	6.32	6.32	0.04470393	102.06	67.26	2.262.08	2.249.70	9.95	
800	0.07	-0.02	0.004	29.67	0.004	48.55	2.54	2.76	0.01799396	44.41	25.12	895.71	895.46	9.95	
900	0.10	-0.09	0.004	26.82	0.004	79.33	3.45	3.67	0.02393423	44.36	29.16	900.24	894.47	9.91	
1000	0.13	-0.12	0.004	27.85	0.004	114.55	4.20	4.45	0.02586959	44.40	25.15	900.38	892.36	9.86	
1100	0.07	-7.12	0.004	21.48	0.004	48.06	2.51	2.75	0.01717866	35.96	20.91	704.03	703.79	10.03	



2. Component Level - Heat Exchanger (TL-MA)



NAME	VALUE
Configuration	
Flow arrangement	Cross flow
Cross flow arrangement	Both fluids unmixed
Thermal resistance through heat tra...	0 K/KW
Cross-sectional area at port A1	$\pi * \text{geo.LTR.D_inlet}^2 / 4$ mm ²
Cross-sectional area at port B1	$\pi * \text{geo.LTR.D_outlet}^2$ mm ²
Cross-sectional area at port A2	$\text{geo.LTR.Width} * \text{geo.LTR.}$ m ²
Cross-sectional area at port B2	$\text{geo.HTR.Width} * \text{geo.HT.}$ m ²
Thermal Liquid 1	
Flow geometry	Flow inside one or more tubes
Number of tubes	$\text{geo.LTR.nTubesPerRowPerCol}$ 29
Total length of each tube	$\text{geo.LTR.Width} * \text{geo.LTR.}$ m
Tube cross section	Rectangular
Tube width	$\text{geo.LTR.Depth} - \text{geo.LT.}$ m
Tube height	$\text{geo.LTR.TubeHeight-geo.}$ m
Pressure loss model	Pressure loss coefficient
Pressure loss coefficient, delta_p/(0...	1.09
Heat transfer coefficient model	Colburn equation
Coefficients [a, b, c] for a*Re^b*Pr^c	[0.012, 0.8033]
Fouling factor	0 K*m ² /KW
Total fin surface area	0 m ²
Fin efficiency	1
Initial thermal liquid pressure	Ambient_P 101.31 kPa
Initial thermal liquid temperature	Ambient_T 20 degC
Moist Air 2	
Flow geometry	Generic
Minimum free-flow area	$\text{geo.LTR.Width} * \text{geo.LTR.}$ m ²
Heat transfer surface area without fi...	$\text{geo.LTR.nTubesPerRowP.}$ m ²

$$dP = K \left(\frac{1}{2} \rho V^2 \right)$$

(pressure loss coefficient)

$$h = Nu \frac{k}{D}$$

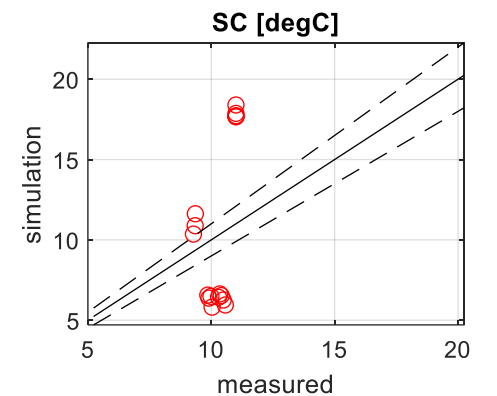
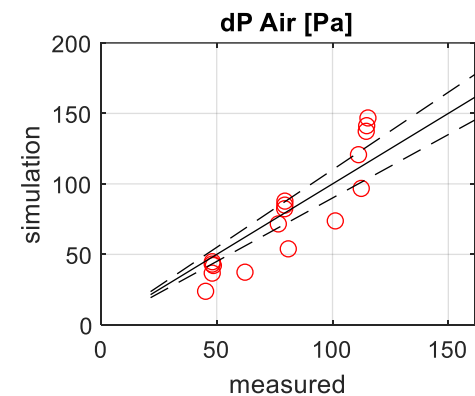
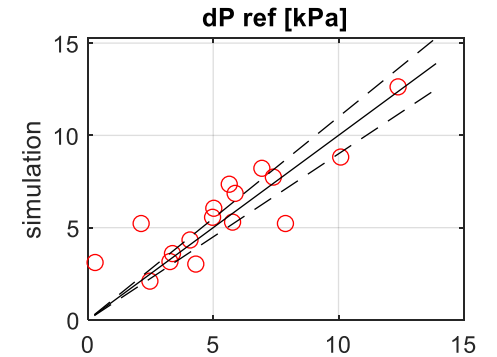
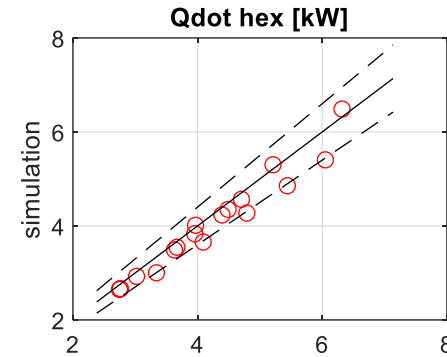
$$Nu = a Re^b Pr^c$$

(Colburn equation)

⊗ each phase

Pressure drop

Heat transfer



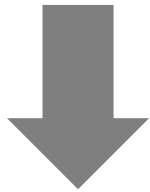
2. Component Level - Compressor(2P)

Geometry
performance

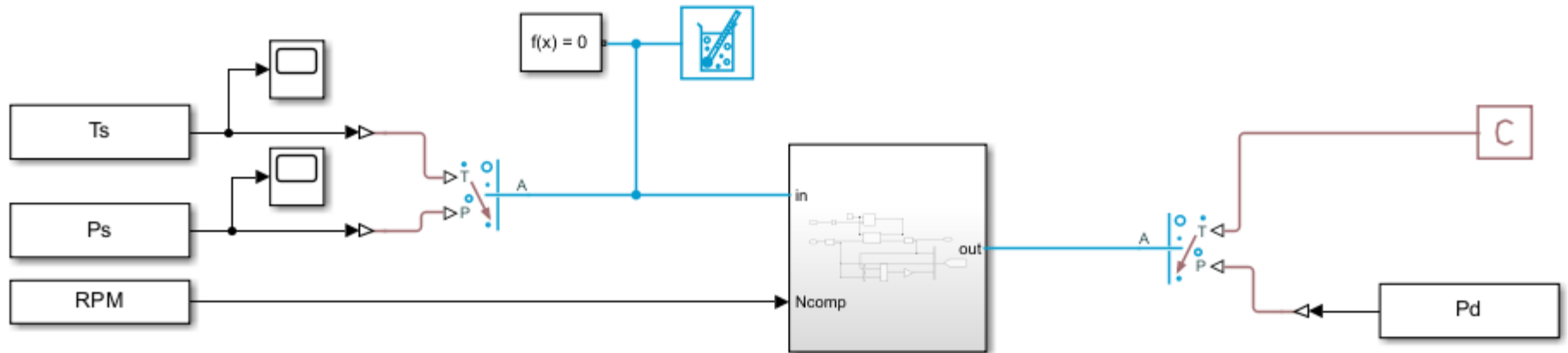


rpm PR η_k

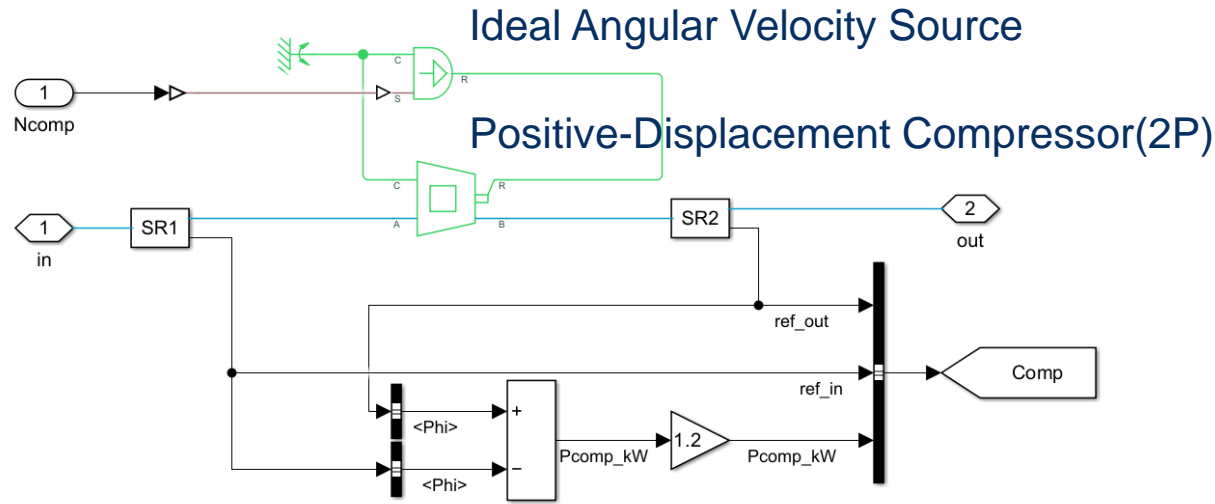
Time	rpm	Pressure Ratio	P_s	P_d	T_s	T_d	T_0	T_{in}	T_{out}	Power	Torque	Torque	Flow rate	Efficiency	Efficiency	Efficiency	
	(rpm)		(bar abs)	(bar abs)	(°C)	(°C)	(°C)	(°C)	(°C)	(kW)	(kg.m)	(Nm)	(kg/min)	(%)	(%)	(%)	
5	1500	3.33	3.00	2.04	10.00	10.00	9.12	57.52	0.00	0.34	0.00	0.00	59.08	0.00	98.3	94.2	90.3
10	5000	3.03	3.00	2.04	10.00	10.00	9.12	57.15	0.00	1.32	0.00	0.00	180.98	0.00	98.5	93.4	84.9
15	5000	3.53	3.00	2.04	10.00	10.00	9.12	57.31	0.00	2.30	0.00	0.00	262.55	0.00	98.0	94.0	82.9
20	1900	5.00	3.00	2.04	10.00	10.00	10.28	96.82	0.00	1.02	0.00	0.00	51.13	0.00	94.7	79.0	49.8
25	2000	5.00	2.00	2.04	10.00	15.00	10.28	75.64	0.00	1.75	0.00	0.00	114.04	0.00	96.8	98.1	92.9
30	5000	5.00	3.00	2.04	10.00	15.00	14.28	74.37	0.00	2.94	0.00	0.00	164.42	0.00	99.1	90.1	84.2
35	7000	5.00	2.00	2.04	10.00	15.00	14.28	78.90	0.00	4.59	0.00	0.00	267.72	0.00	96.8	98.8	97.1
40	9000	5.00	2.00	2.04	10.00	15.00	14.28	79.51	0.00	6.49	0.00	0.00	341.84	0.00	96.8	98.7	97.0
45	10000	5.00	3.00	2.04	10.00	15.00	14.28	82.30	0.00	8.58	0.00	0.00	360.70	0.00	96.5	93.9	83.4
50	2000	5.67	3.00	2.04	10.00	20.00	19.29	95.87	0.00	2.18	0.00	0.00	109.21	0.00	98.0	94.9	90.2
55	3000	6.67	3.00	2.04	10.00	20.00	19.29	90.18	0.00	3.49	0.00	0.00	138.30	0.00	94.1	98.1	90.6
60	7000	6.67	3.00	2.04	10.00	20.00	19.29	94.28	0.00	4.98	0.00	0.00	256.58	0.00	96.2	94.9	90.8
65	9000	6.67	2.00	2.04	10.00	20.00	19.29	93.28	0.00	6.59	0.00	0.00	344.50	0.00	96.8	93.9	90.5
70	10000	6.67	3.00	2.04	10.00	20.00	19.29	96.64	0.00	7.58	0.00	0.00	349.54	0.00	96.5	91.0	83.7
75	3000	8.33	3.00	2.04	10.00	25.00	24.47	100.39	0.00	2.57	0.00	0.00	103.11	0.00	93.8	99.5	91.3
80	5000	8.33	3.00	2.04	10.00	25.00	24.47	104.08	0.00	4.00	0.00	0.00	178.00	0.00	91.3	94.8	91.9
85	7000	8.33	3.00	2.04	10.00	25.00	24.47	103.69	0.00	5.91	0.00	0.00	250.32	0.00	92.4	92.9	88.2
90	8000	9.33	3.00	2.04	10.00	25.00	24.47	103.33	0.00	6.99	0.00	0.00	268.58	0.00	94.4	96.5	94.4
95	10000	9.33	3.00	2.04	10.00	25.00	24.47	108.83	0.00	8.42	0.00	0.00	336.72	0.00	91.1	77.7	72.7



Modeling
- Environment
- HEX

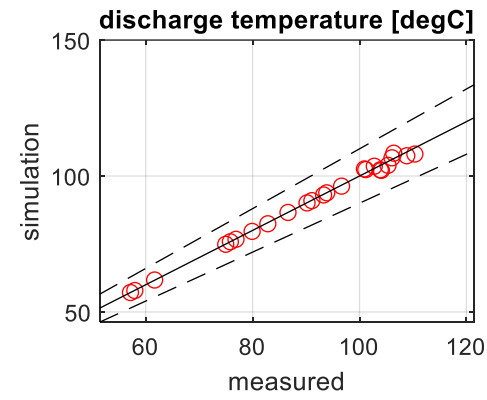
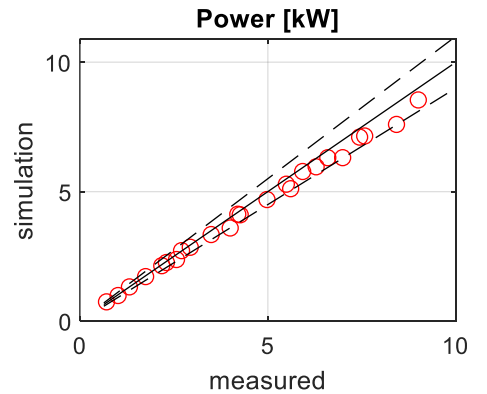
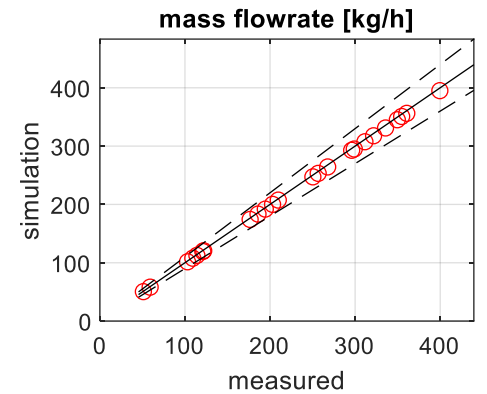


2. Component Level - Compressor(2P)



Mass flowrate

Power



NAME	VALUE
Displacement	
Displacement specification	Volumetric displacement
> Displacement volume	geo.Comp.Displacement ... cm ³ /rev
Efficiency	
Efficiency specification	Tabulated
Thermodynamic model	Isentropic
> Isentropic efficiency table, eta_isen(...)	geo.Comp.iseneff_table <5x7 double>
> Pressure ratio vector, pr	geo.Comp.Pratio_vector <5x1 double>
> Shaft speed vector, w	geo.Comp.RPM_vector <... rpm
> Volumetric efficiency table, eta_vol(...)	geo.Comp.Voleff_table <5x7 double>
Nominal Conditions	
Parameters	
> Mechanical efficiency	1
> Inlet area at port A	pi * geo.Comp.D_inlet ^2 /4 mm ²
> Outlet area at port B	pi * geo.Comp.D_outlet ^2... mm ²
Report when fluid is not fully vapor	None

$$\dot{m}_{comp} = \frac{N}{60} \rho_{in} V_D \eta_v$$

$$P_{flow} = \frac{N}{60} P_{in} V_{in} \left(\frac{n}{n-1} \right) \left(\left(\frac{P_{out}}{P_{in}} \right)^{\frac{n-1}{n}} - 1 \right)$$

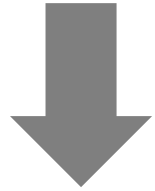
$$P_{comp} = P_{flow} / \eta_k$$

n : polytropic exponent
 $1 < n \leq \gamma = C_p / C_v$

2. Component Level

- Air & coolant flowrate

Measurement



Table

- Cooling fan
- Blower
- Water pump

Incompressible fluid

$$\dot{m}_{coolant} = f(N_{ewp}, 3WV, T_{coolant})$$

$$P_{ewp} = g(N_{ewp}, 3WV, T_{coolant})$$

Compressible fluid

$$\dot{m}_{fan} = f(Fduty, V_{speed}, AAF)\rho_{air}$$

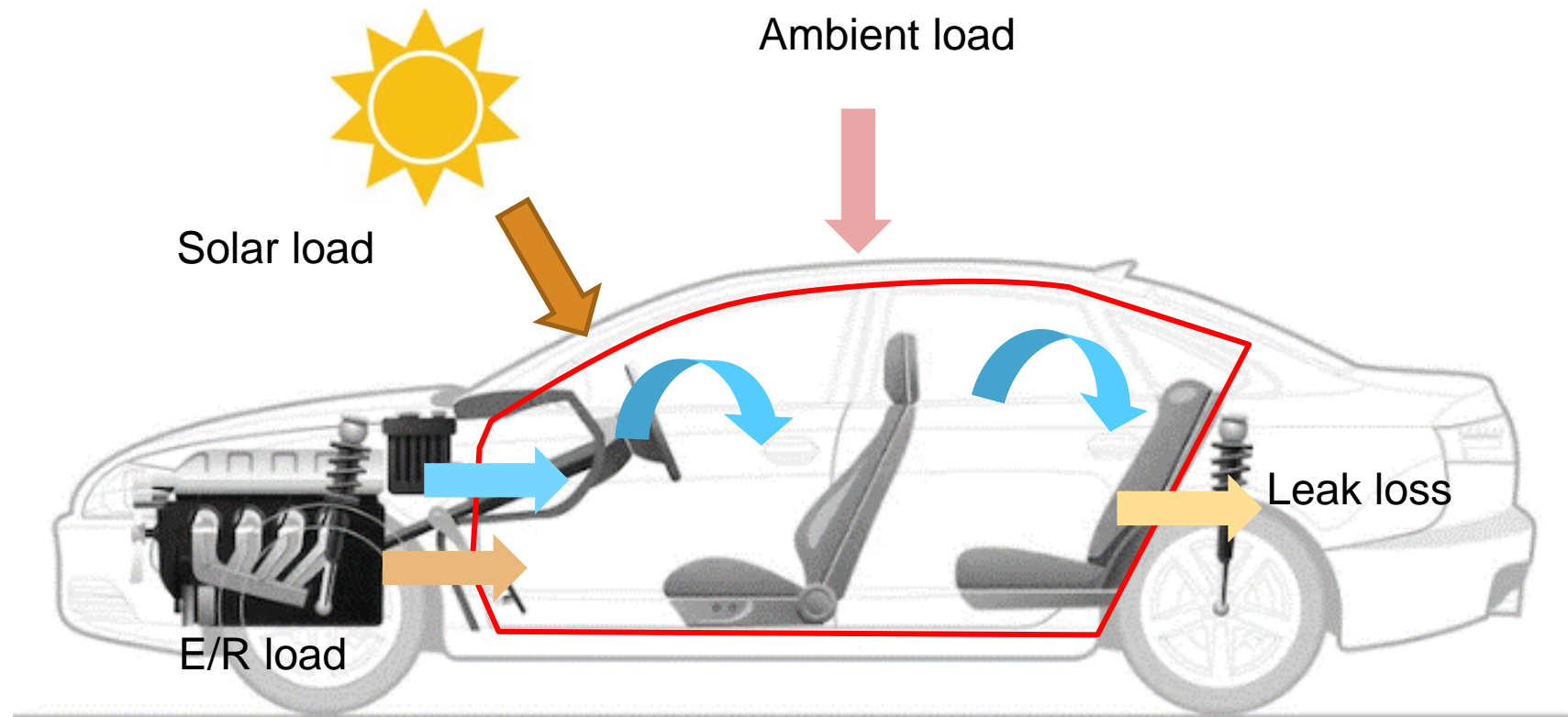
$$P_{fan} = g(Fduty, V_{speed}, AAF)$$

$$\dot{m}_{blwr} = f(V_{blwr}, intake, V_{speed}, mode)\rho_{air}$$

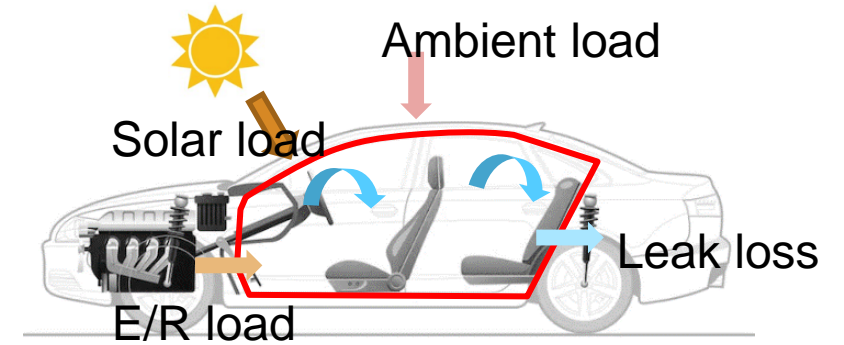
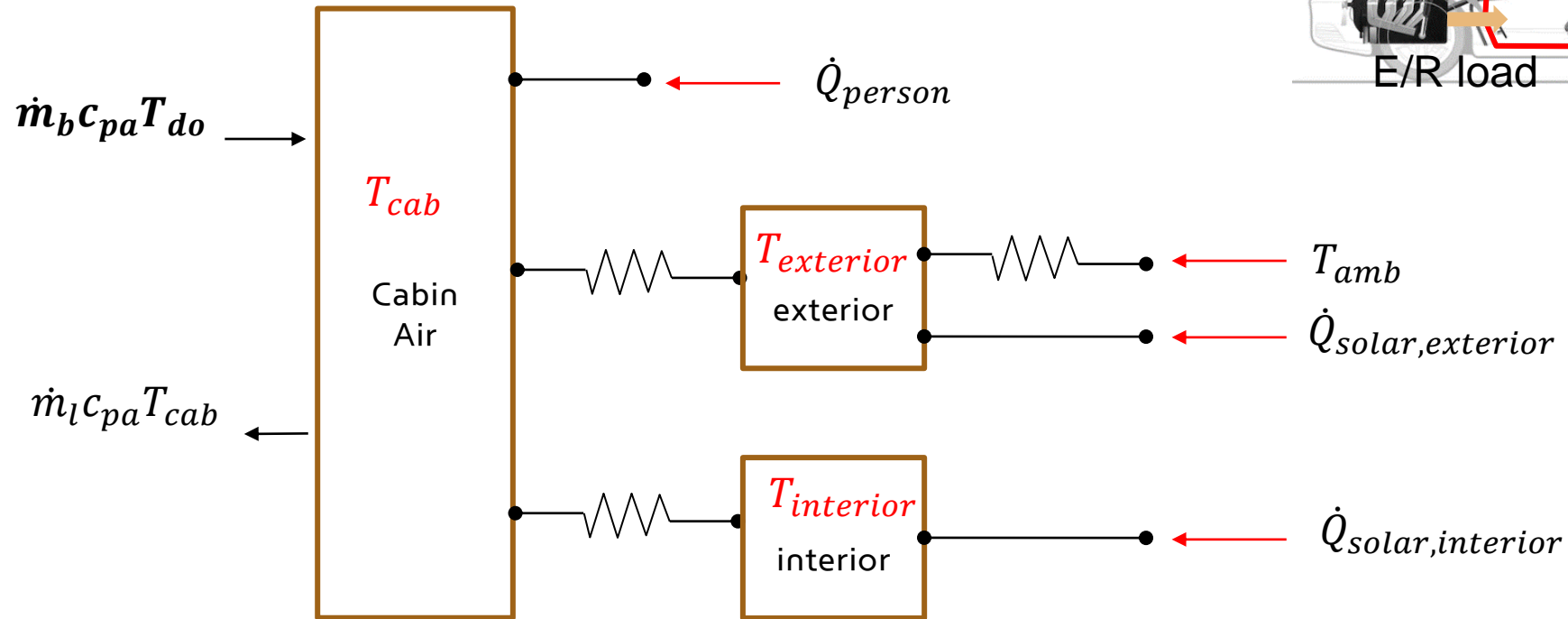
$$P_{blwr} = g(V_{blwr}, intake, V_{speed}, mode)$$

2. Component Level

- Cabin



2. Component Level - Cabin



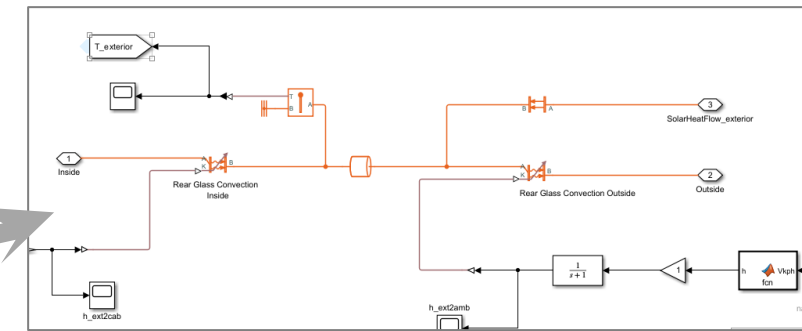
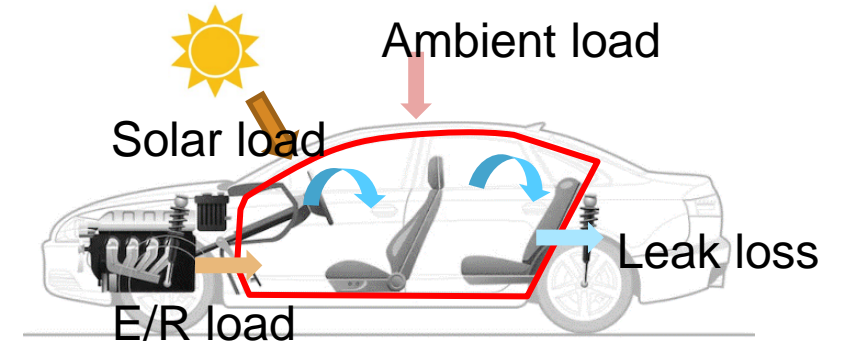
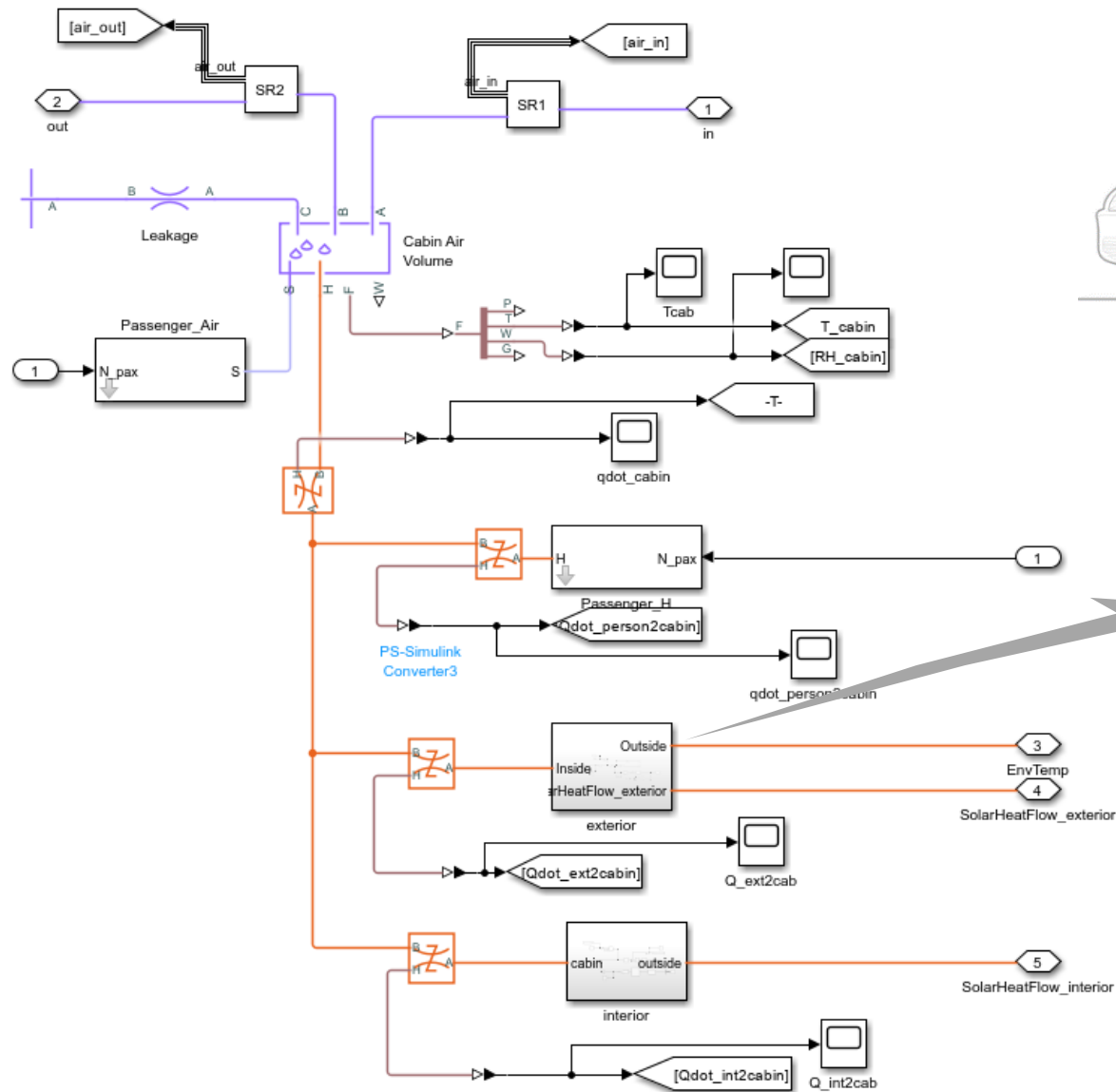
2. Component Level - Cabin

Cabin Air

Passenger

exterior

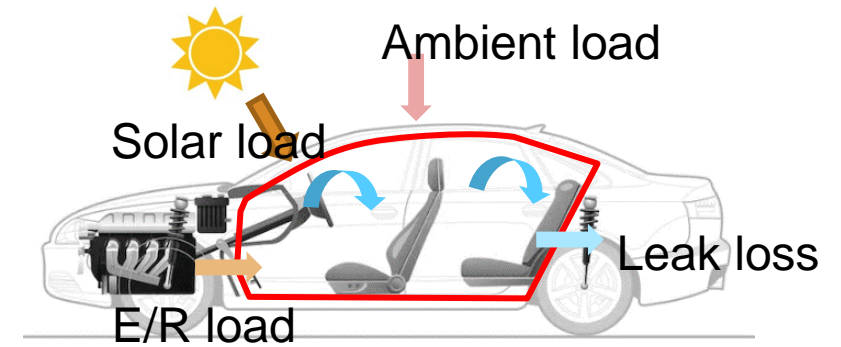
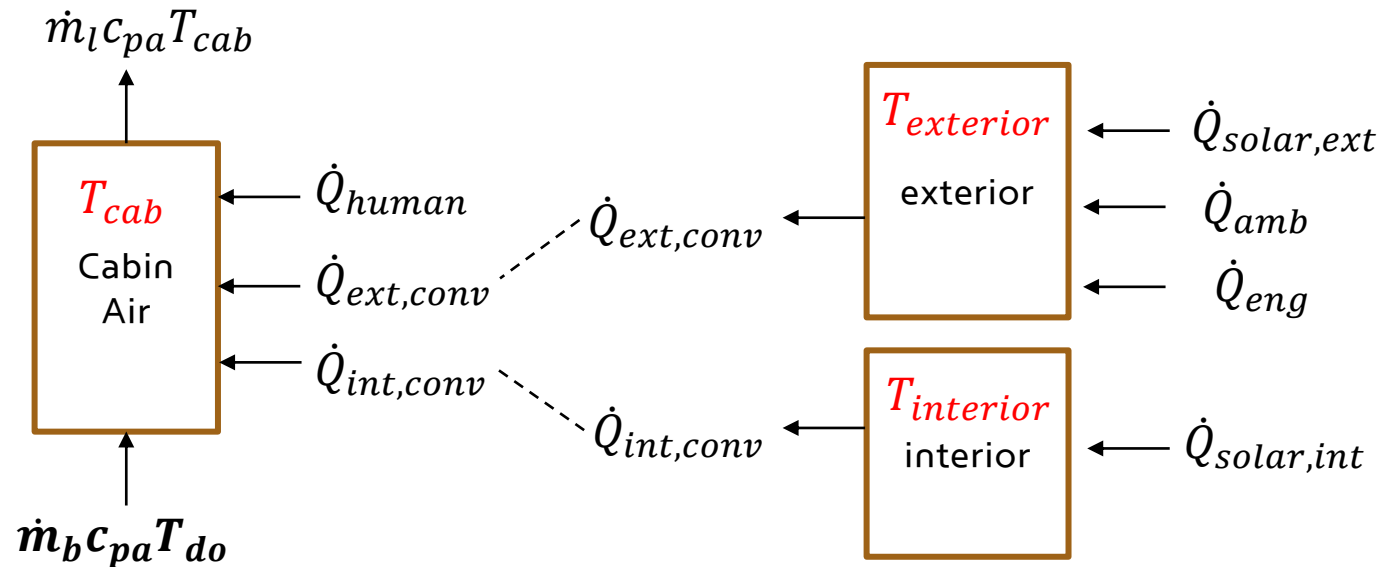
interior



Thermal mass

- Convective heat transfer
- Conductive heat transfer
- Radiant heat transfer

2. Component Level - Cabin



$$MC \frac{dT}{dt} = \sum \dot{Q}_k$$

$$\dot{Q} = hA(T_2 - T_1)$$

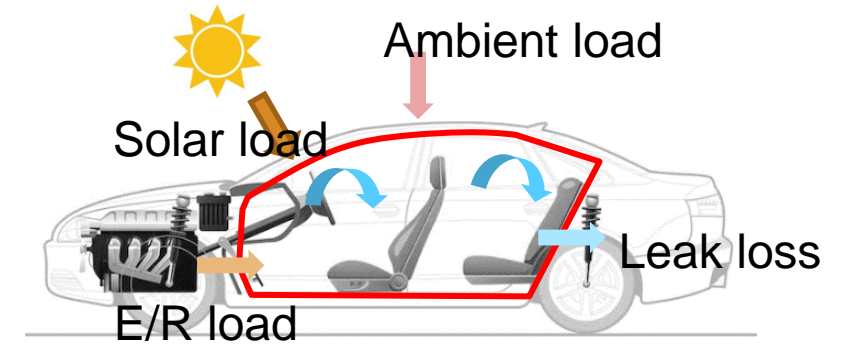
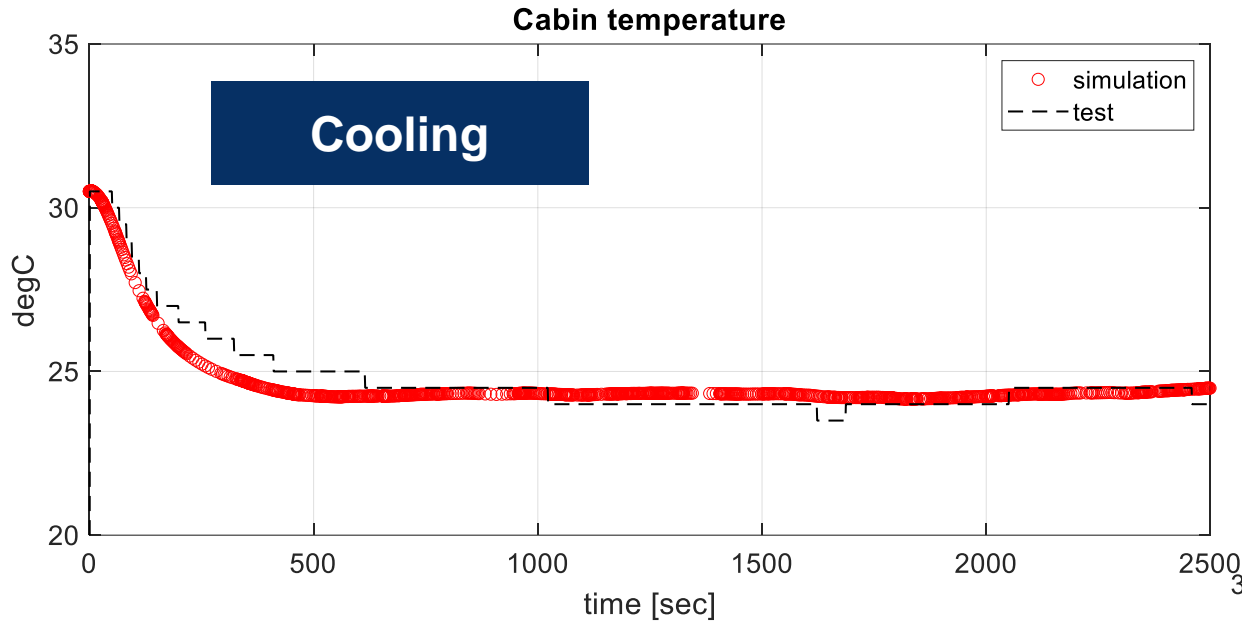
$$\dot{Q} = \frac{kA}{l}(T_2 - T_1)$$

$$\frac{dT_{cab}}{dt} = \frac{1}{m_{cab}c_{p,cab}} (\dot{m}_b c_{pa} (T_{a,do} - T_{cab}) + hA_e (T_{ext} - T_{cab}) + hA_i (T_{int} - T_{cab}) + \dot{Q}_{human} - \dot{m}_{leak} c_{pa} T_{cab})$$

$$\frac{dT_{ext}}{dt} = \frac{1}{m_{ext}c_{p,ext}} (\alpha_{s,ext} \dot{Q}_{solar} + hA_{amb} (T_{amb} - T_{ext}) - hA_e (T_{ext} - T_{cab}) + \dot{Q}_{eng})$$

$$\frac{dT_{int}}{dt} = \frac{1}{m_{int}c_{p,int}} (\alpha_{s,int} \dot{Q}_{solar} - hA_i (T_{int} - T_{cab}))$$

2. Component Level - Cabin



7 parameters

$$m_{cab}C_{p,cab}$$

$$m_{ext}C_{p,ext}$$

$$m_{int}C_{p,int}$$

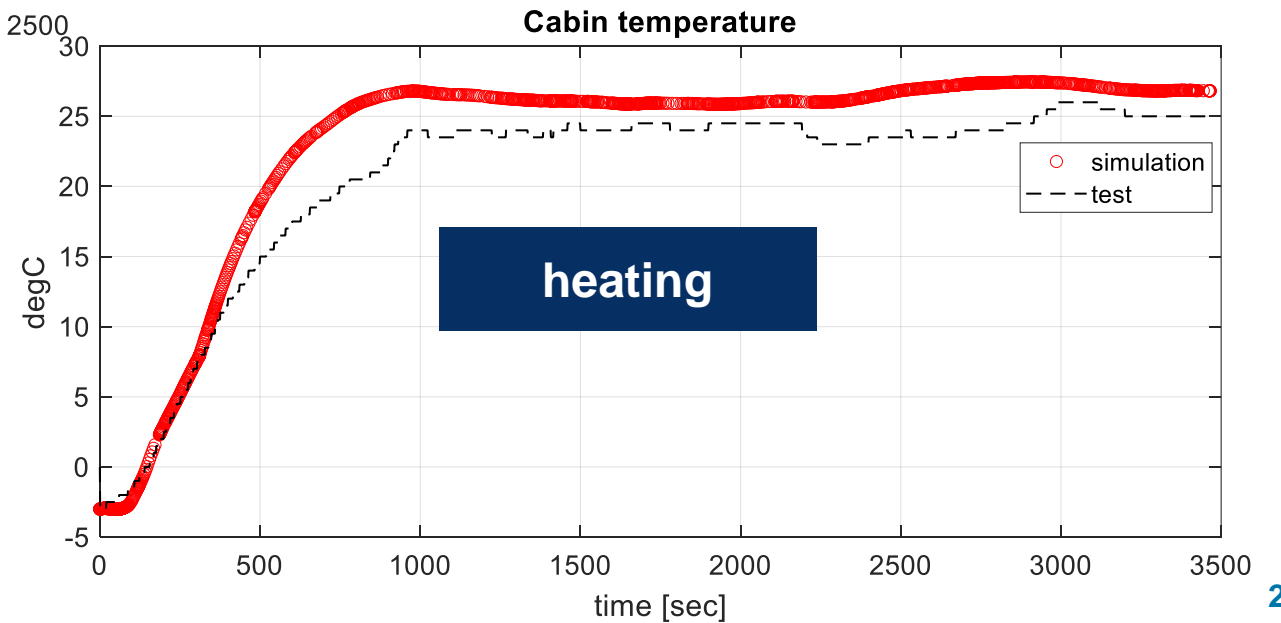
$$hA_e$$

$$hA_i$$

$$hA_{amb}$$

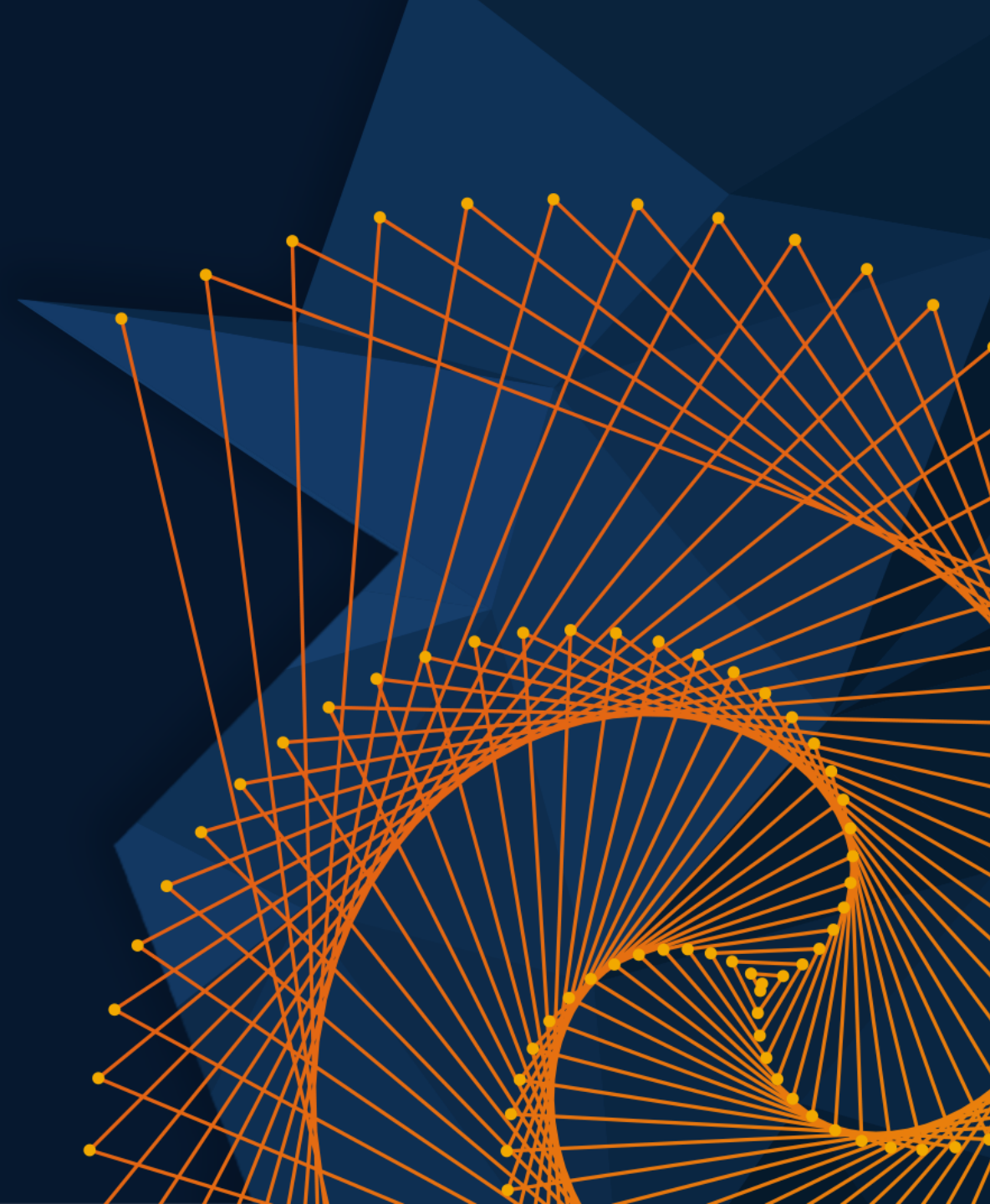
$$h_{s,ext}$$

$$h_{s,int}$$

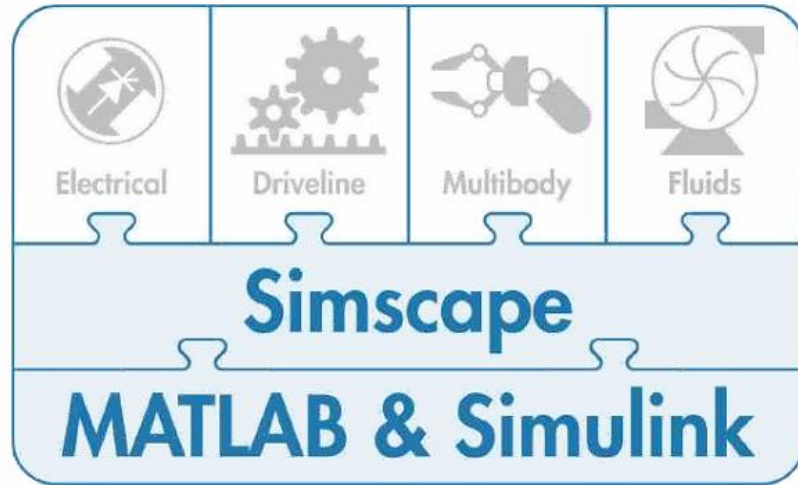


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2. Component level
- 3. System level**
4. Control logic & Verification
5. Conclusion

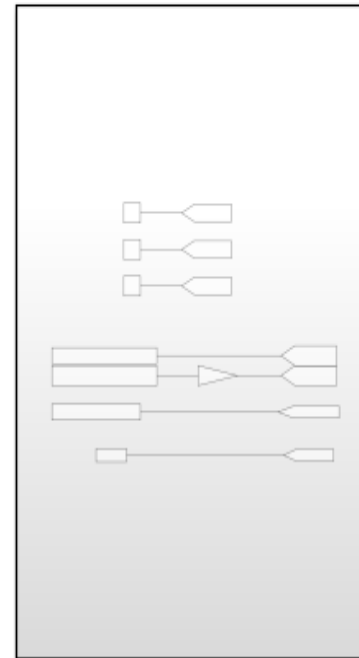


3. System Level - Plant

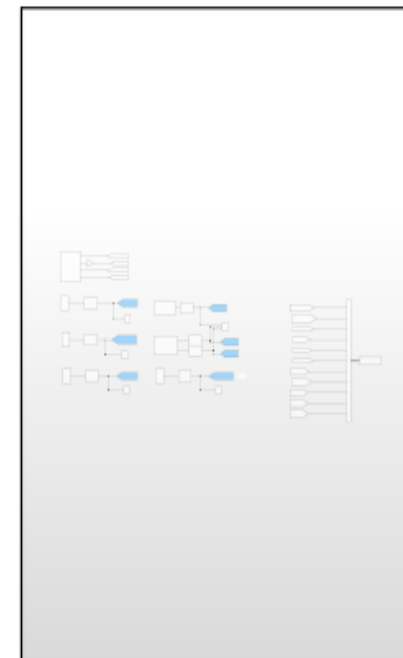


Thermal circuit
- Cooling
- Air conditioning

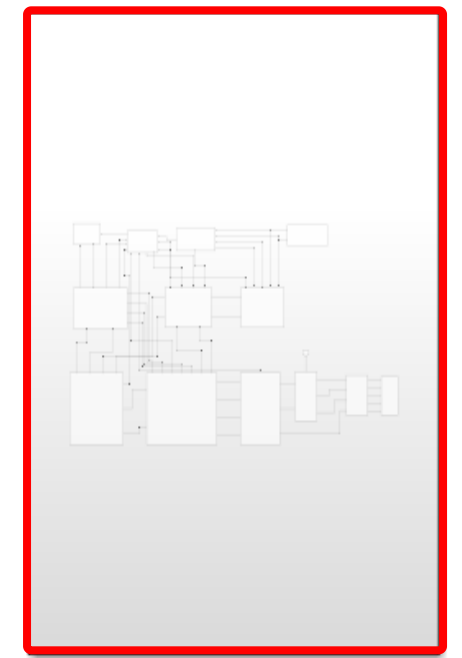
Simulink & Simscape



Environment



Controller

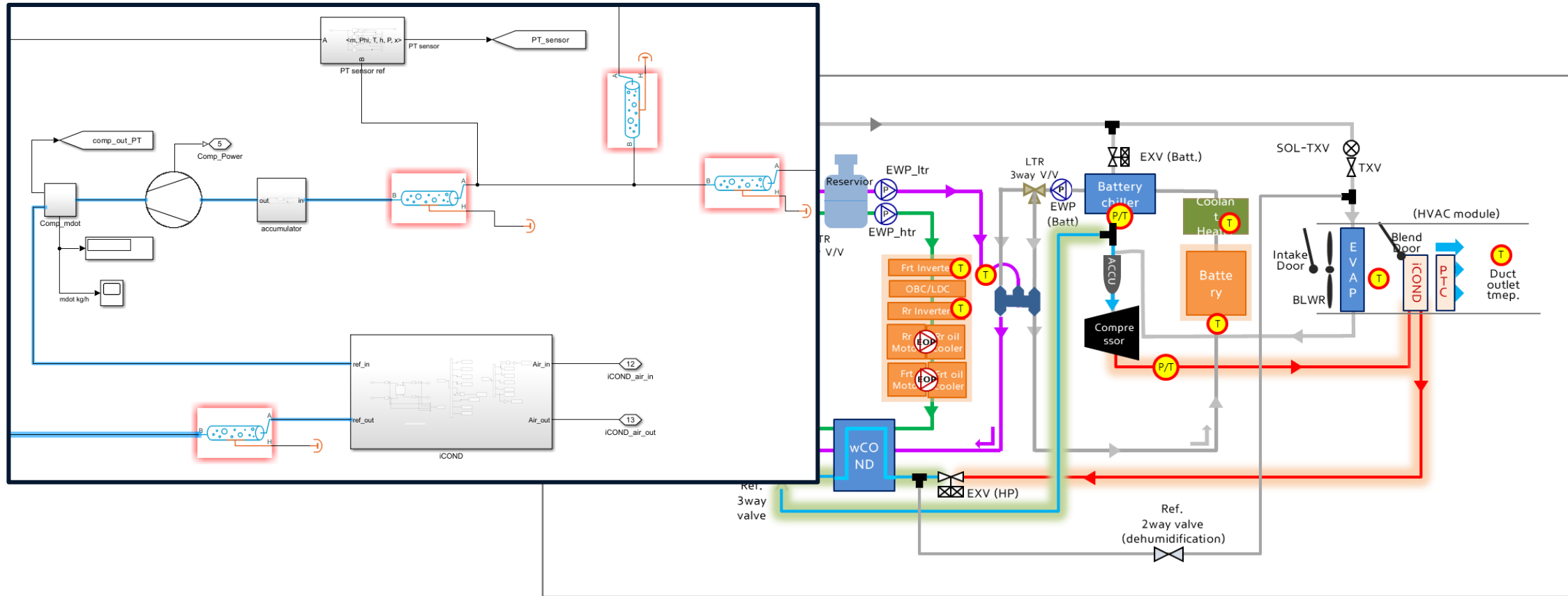


Plant

3. System Level

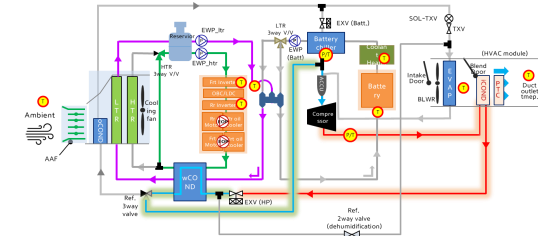
- integration for thermal circuit

Pipe (2P,TL)

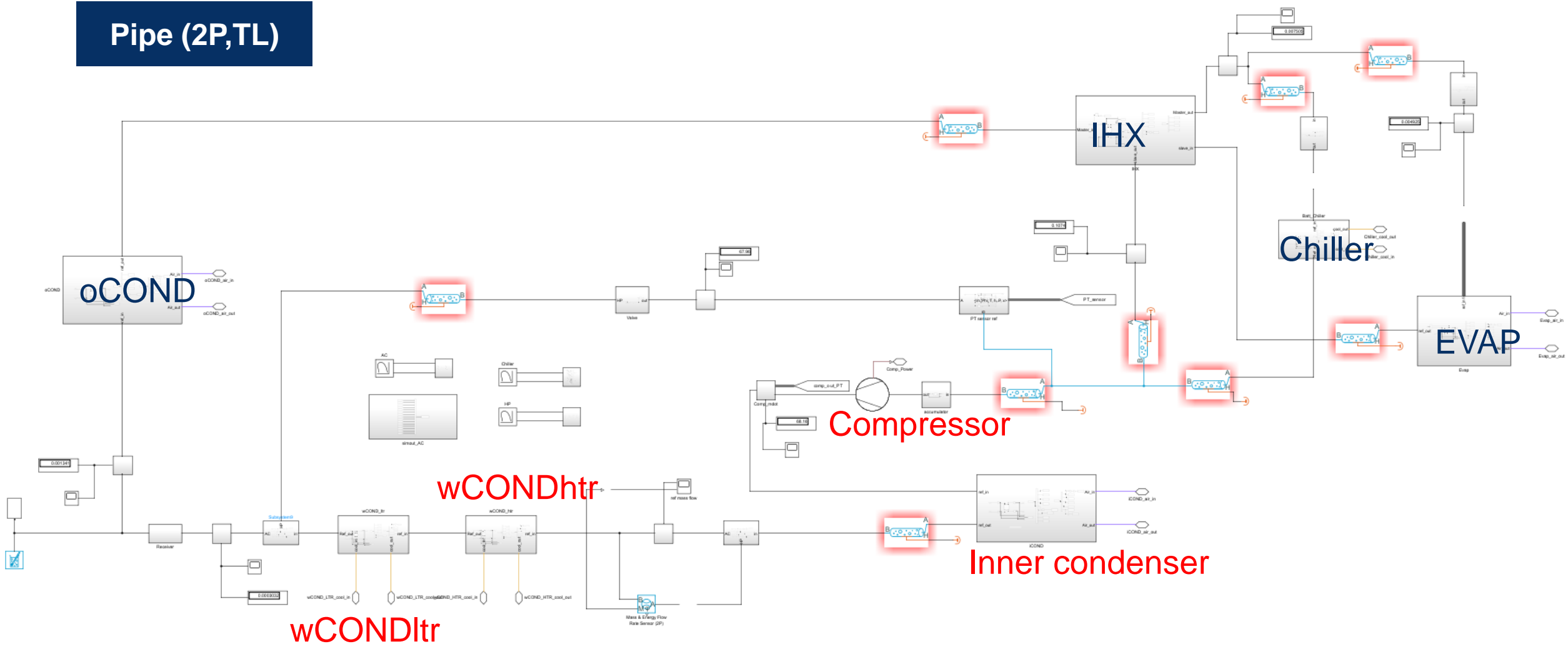


3. System Level

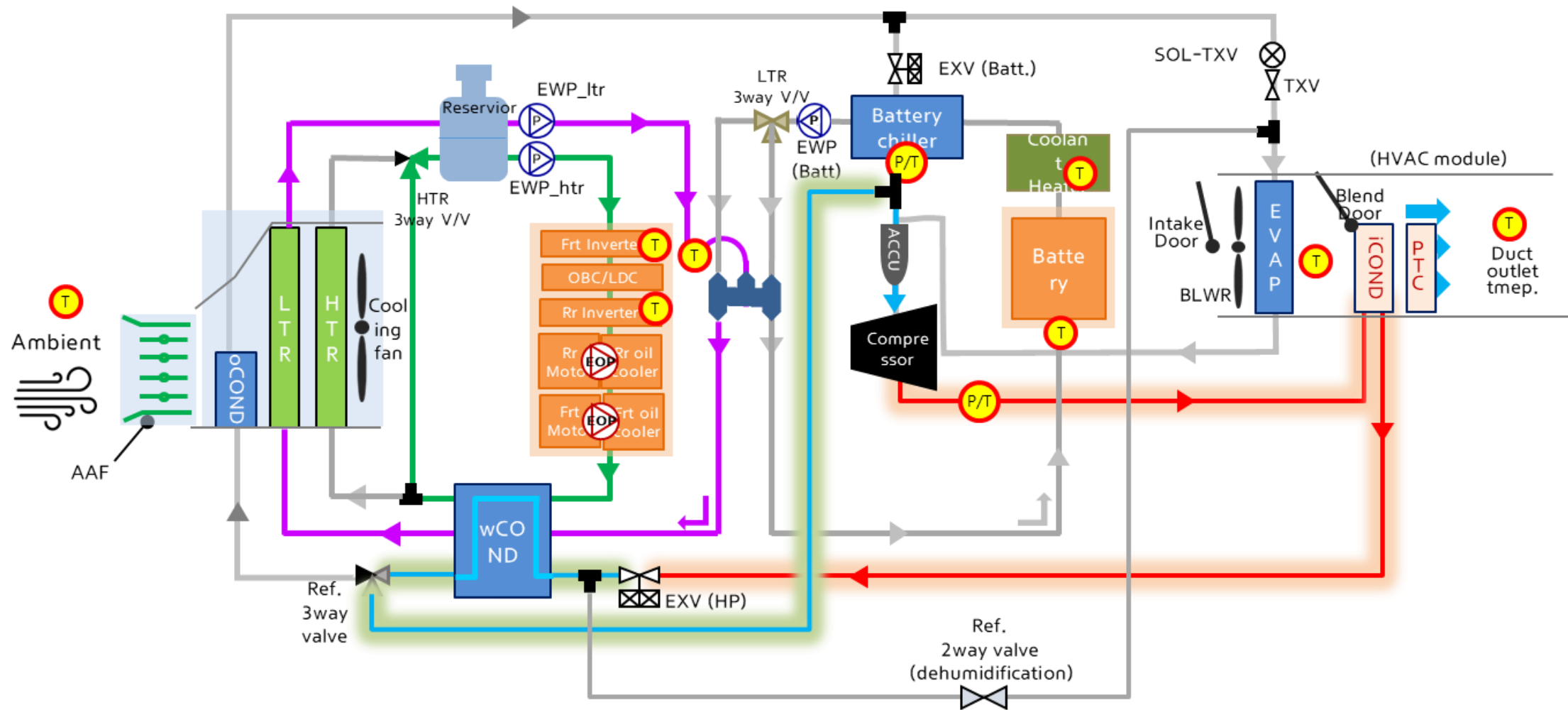
- Heat pump (2P-MA,2P-TL, TXV, EXV, Compressor)



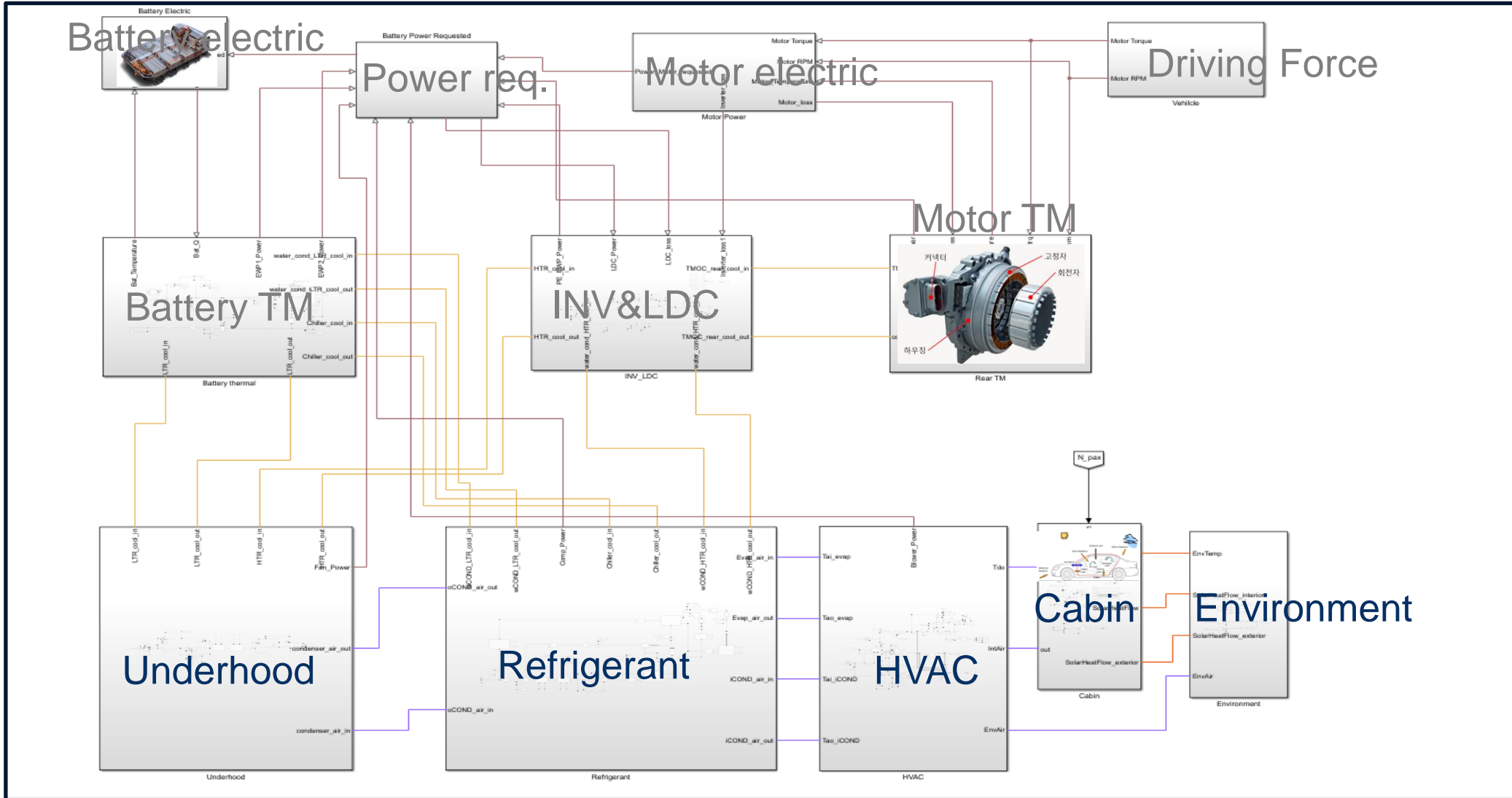
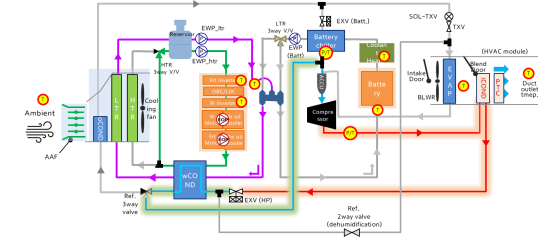
Pipe (2P,TL)



3. System Level - Thermal circuit

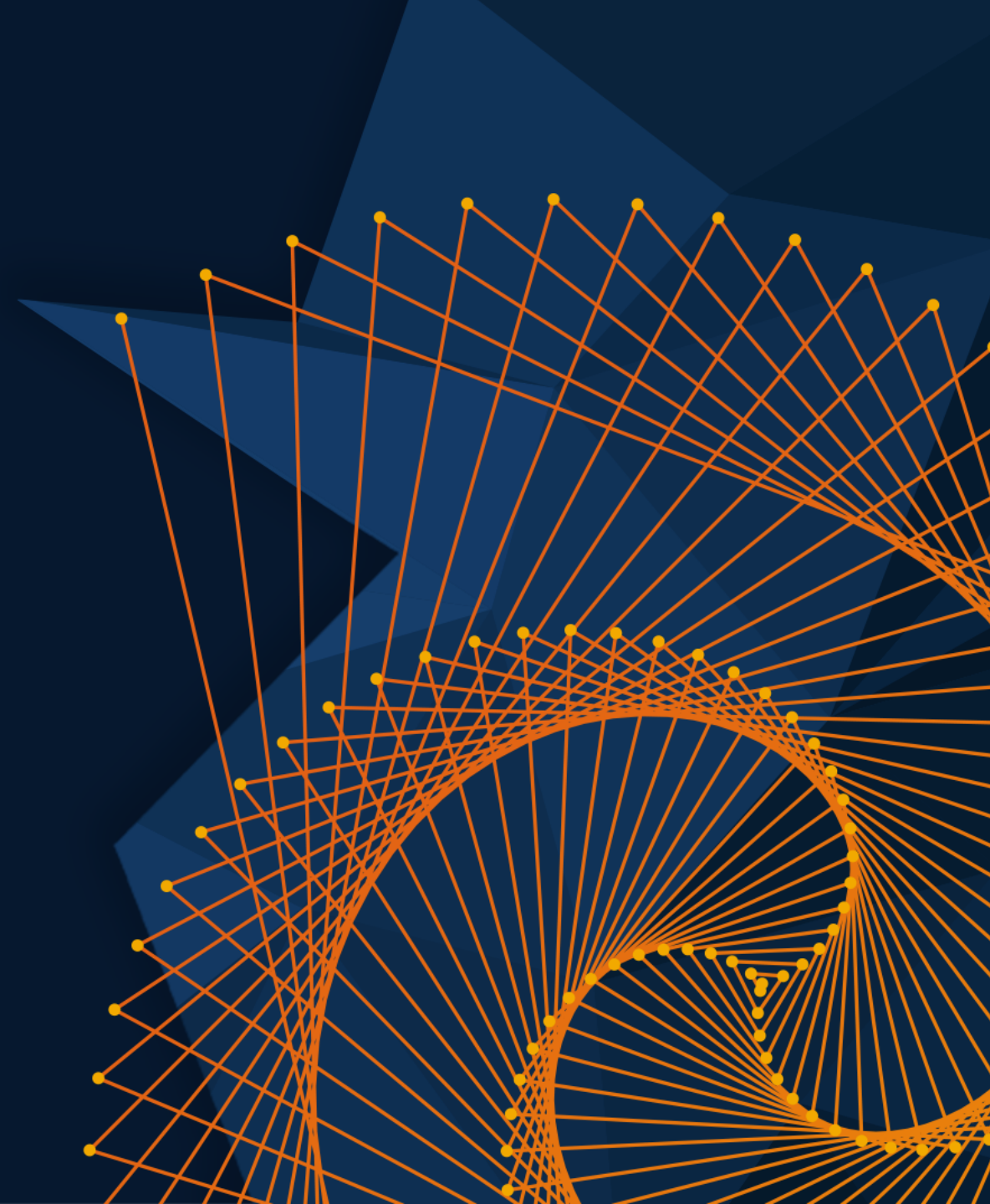


3. System Level - Thermal circuit

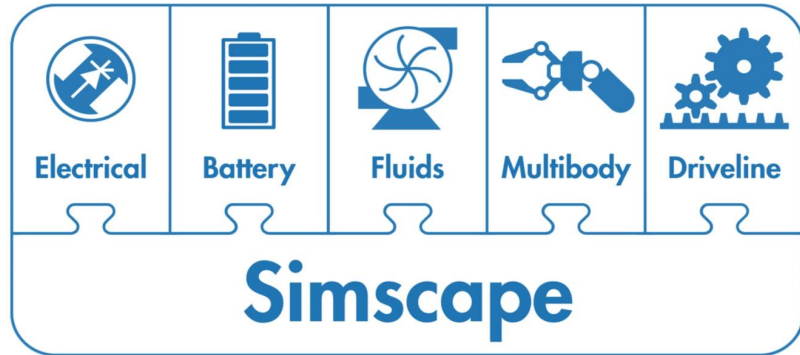


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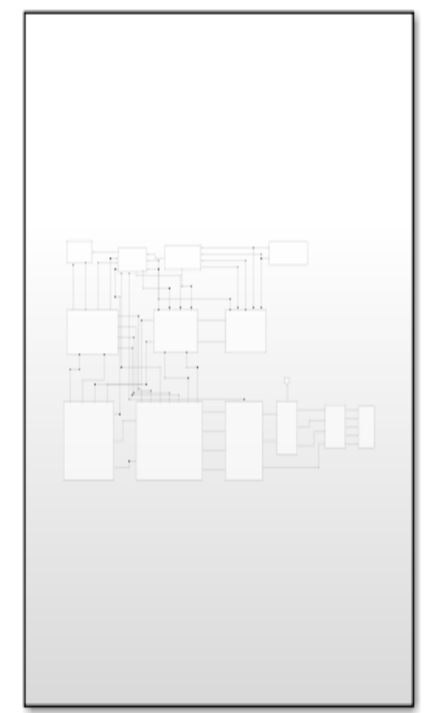
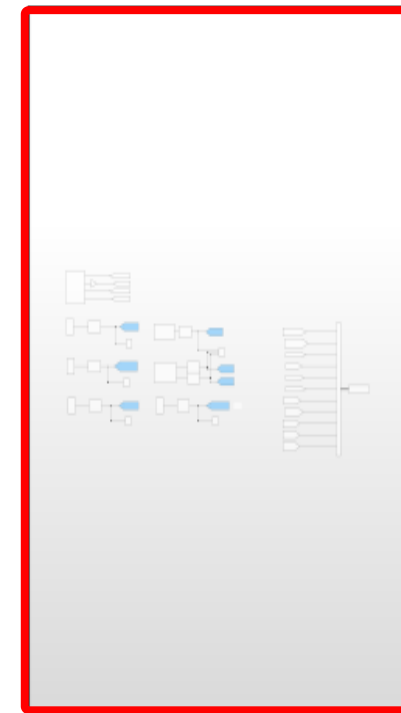
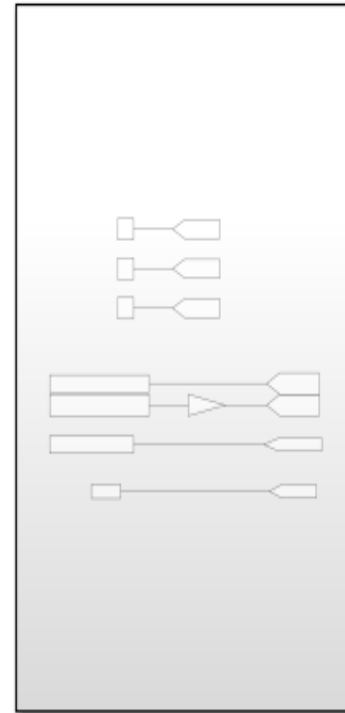


4. Control logic & Verification

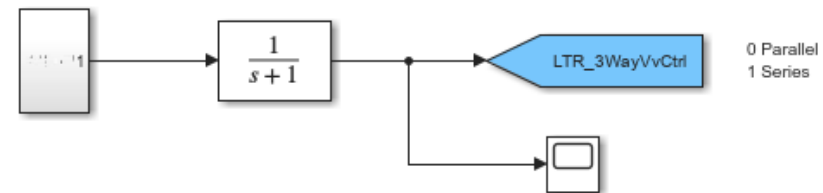
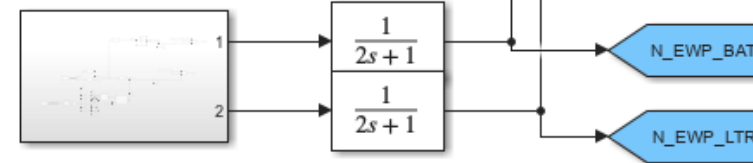
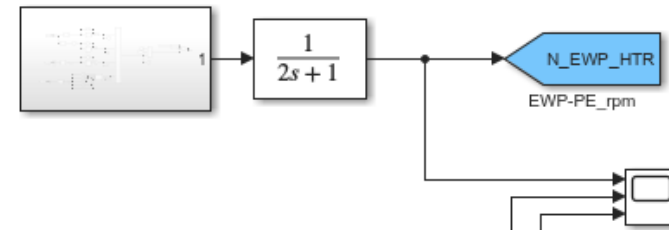
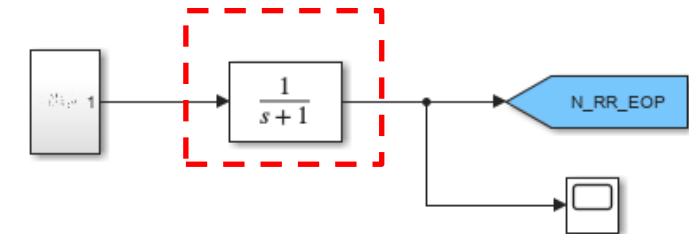
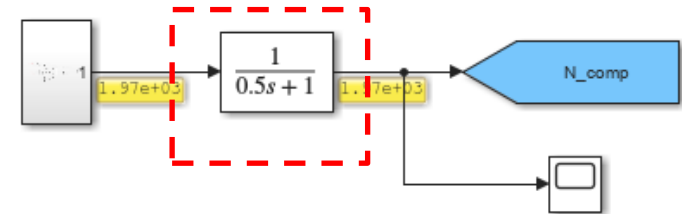
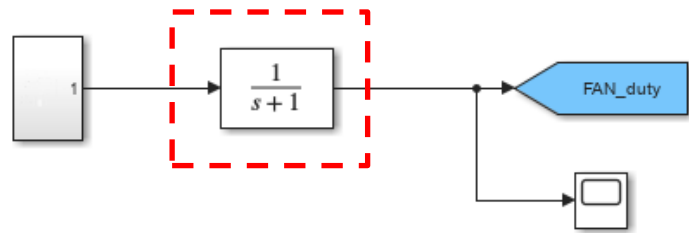
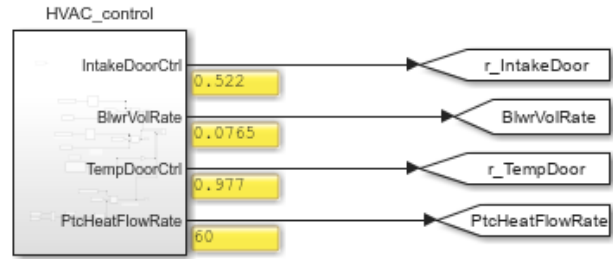


Discrete & Continuous

- Plant : continuous
- Controller : discrete ?



4. Control logic & Verification

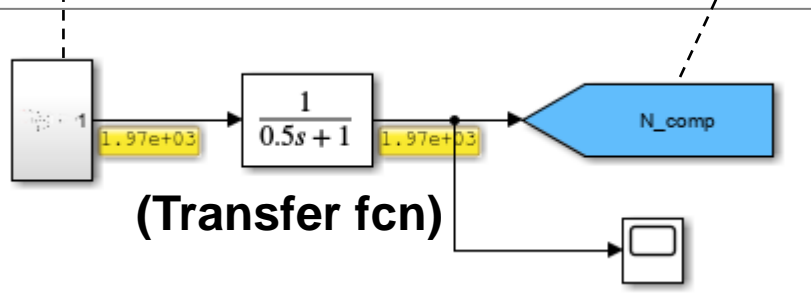


4. Control logic & Verification

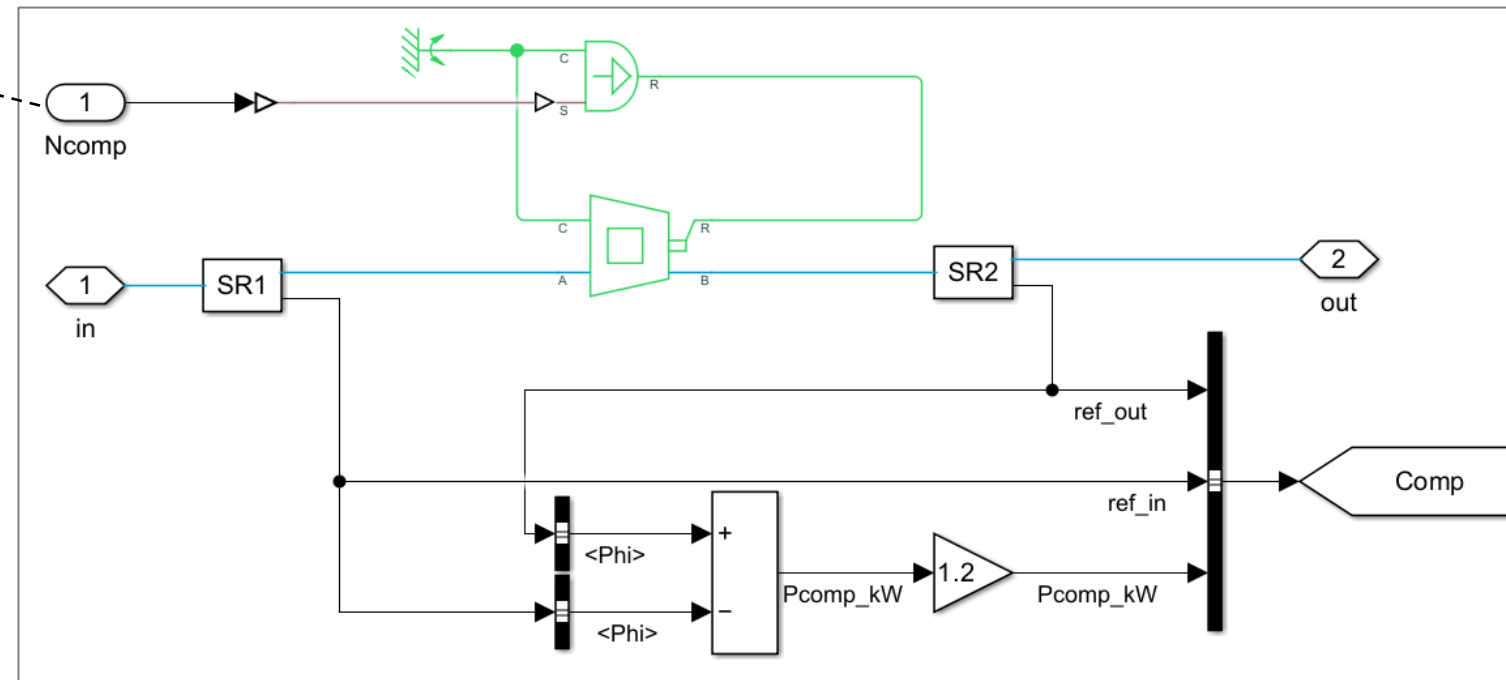
Controller

- Logic : discrete

- Signal : continuous



Plant



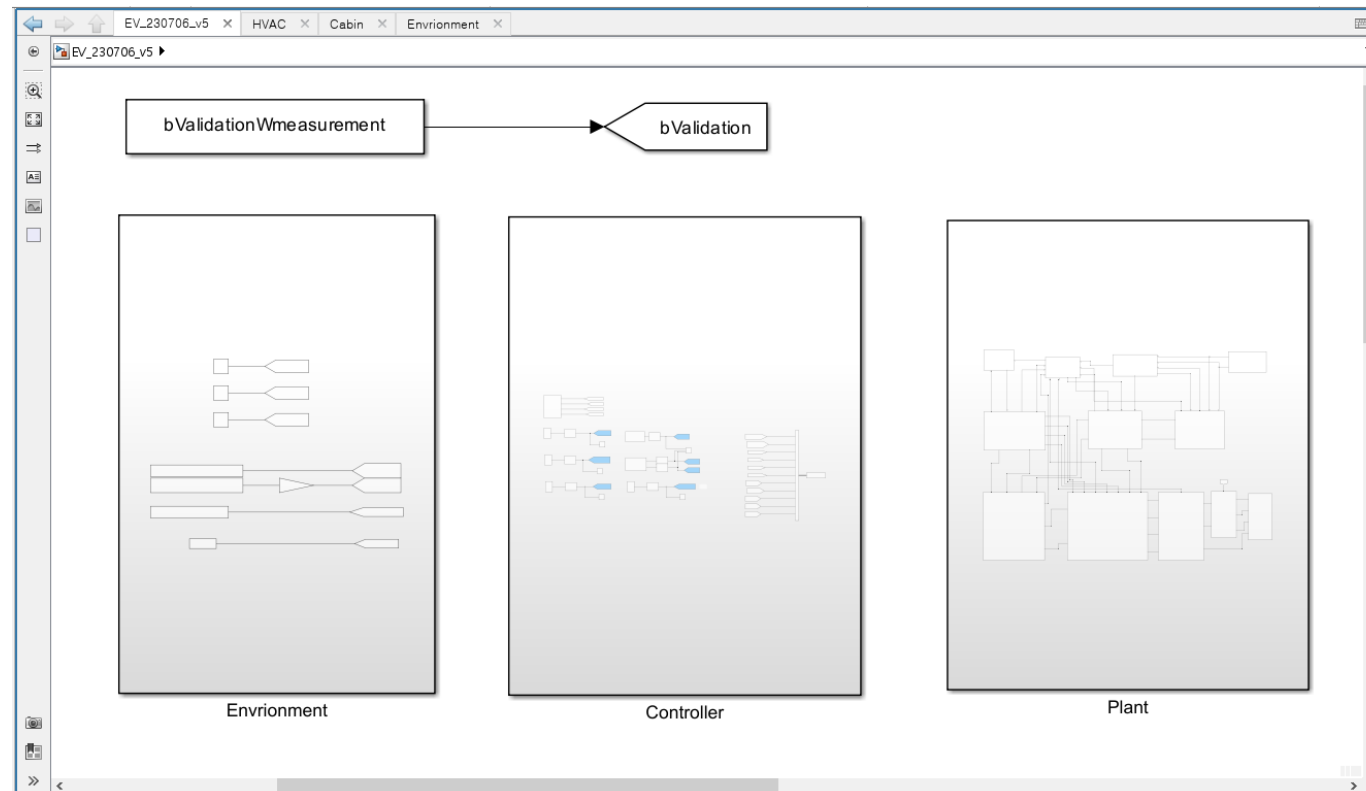
4. Control logic & Verification

Run time

- compile + initializing : 3.5minute + 1.5minute (too slow)
- after then, the simulation time to real time is 1/3

Compiling : Analyzing equation systems for Simscape physical networks: Started

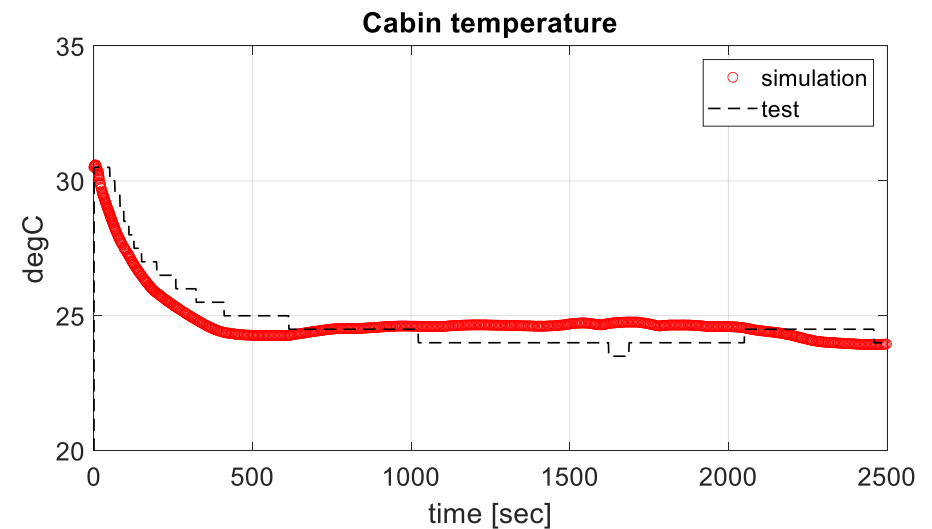
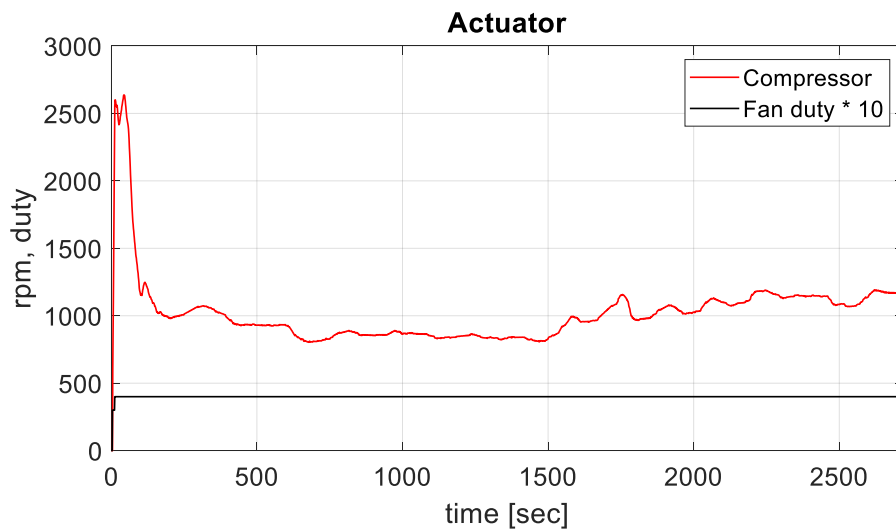
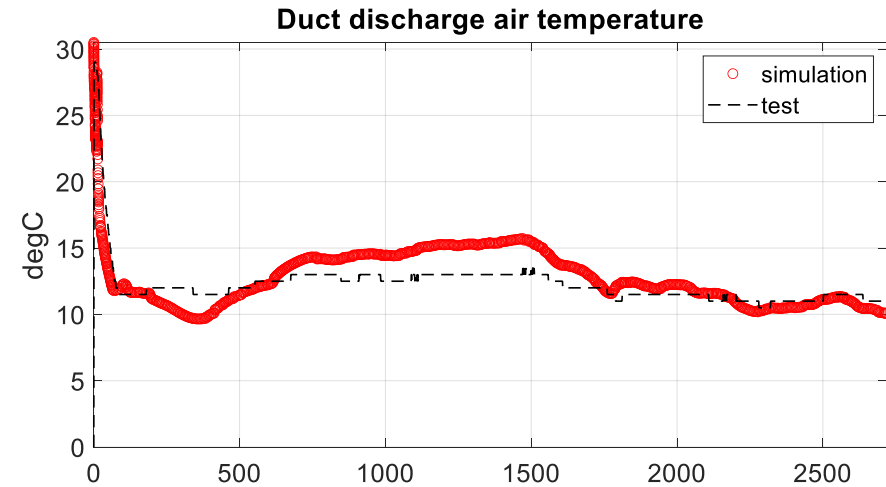
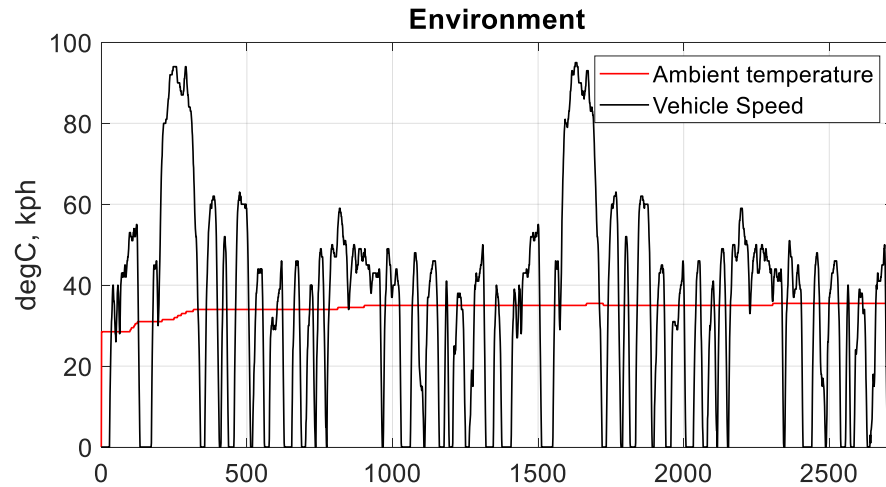
Running : Initializing equation systems for Simscape physical networks: Started



4. Control logic & Verification

- Control input based on experiment : Compressor, cooling fan, EWP, TXV

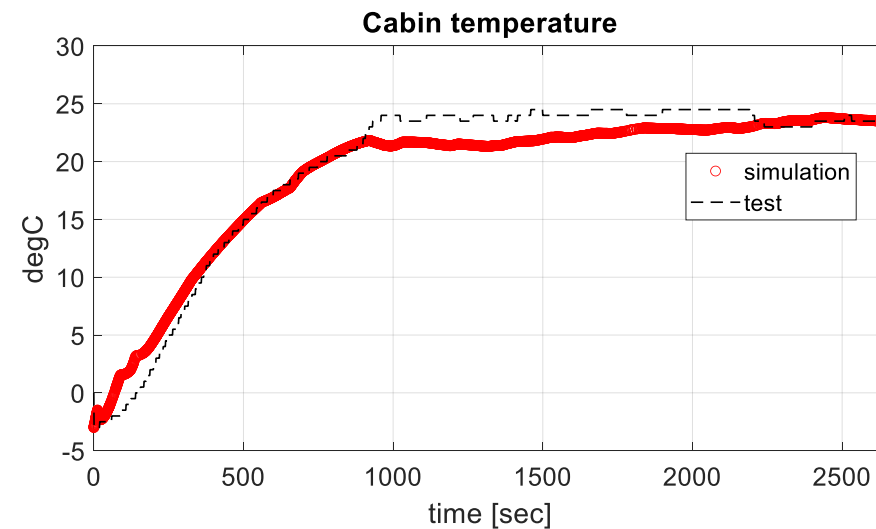
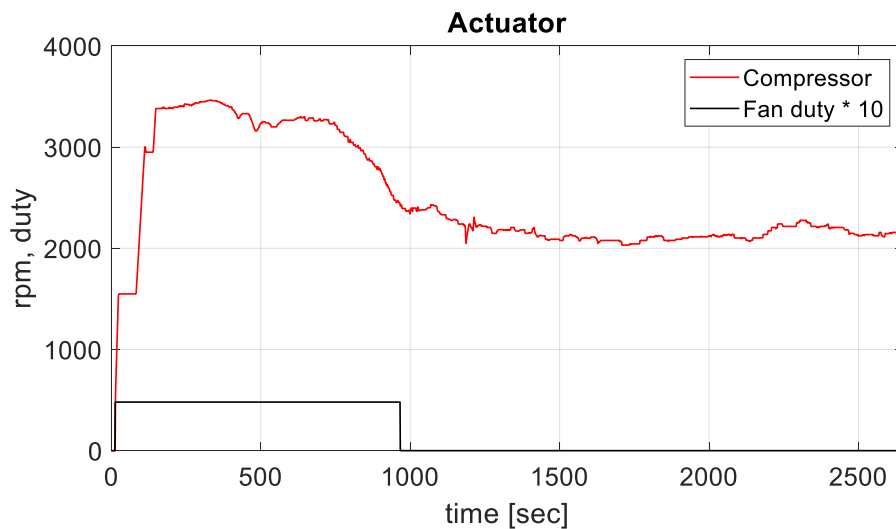
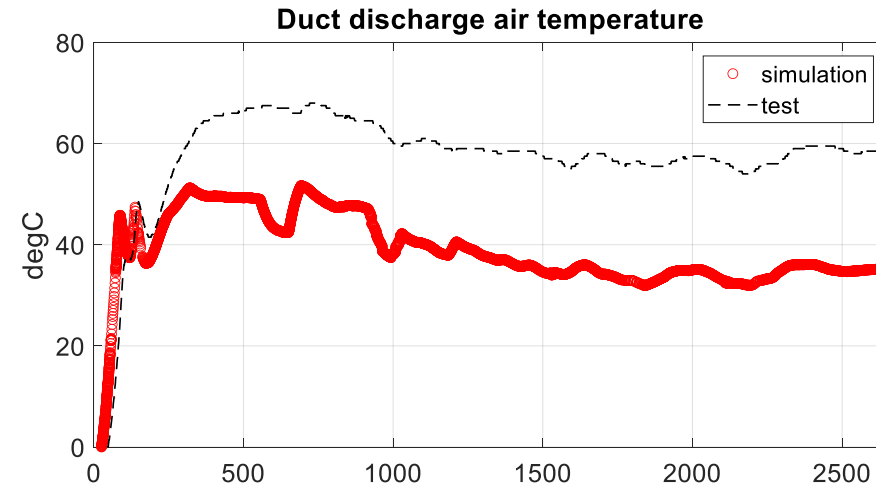
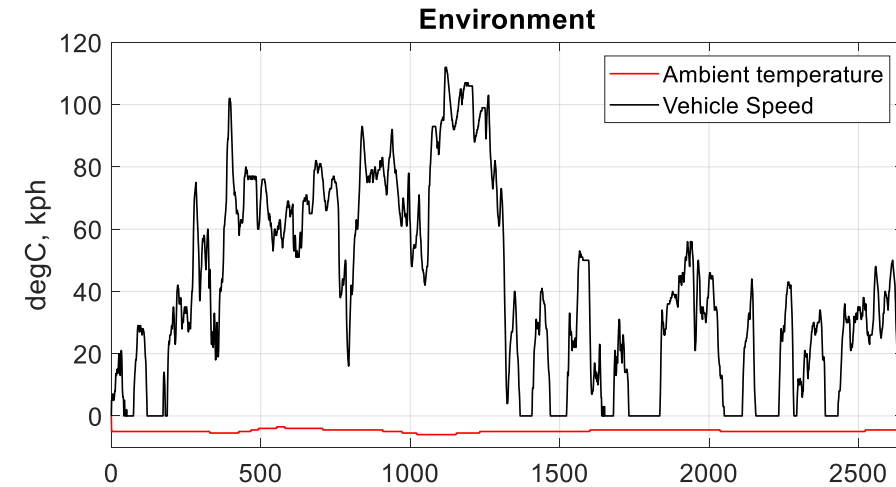
Simulation (Cooling mode around 35°C, 850W/m²)



4. Control logic & Verification

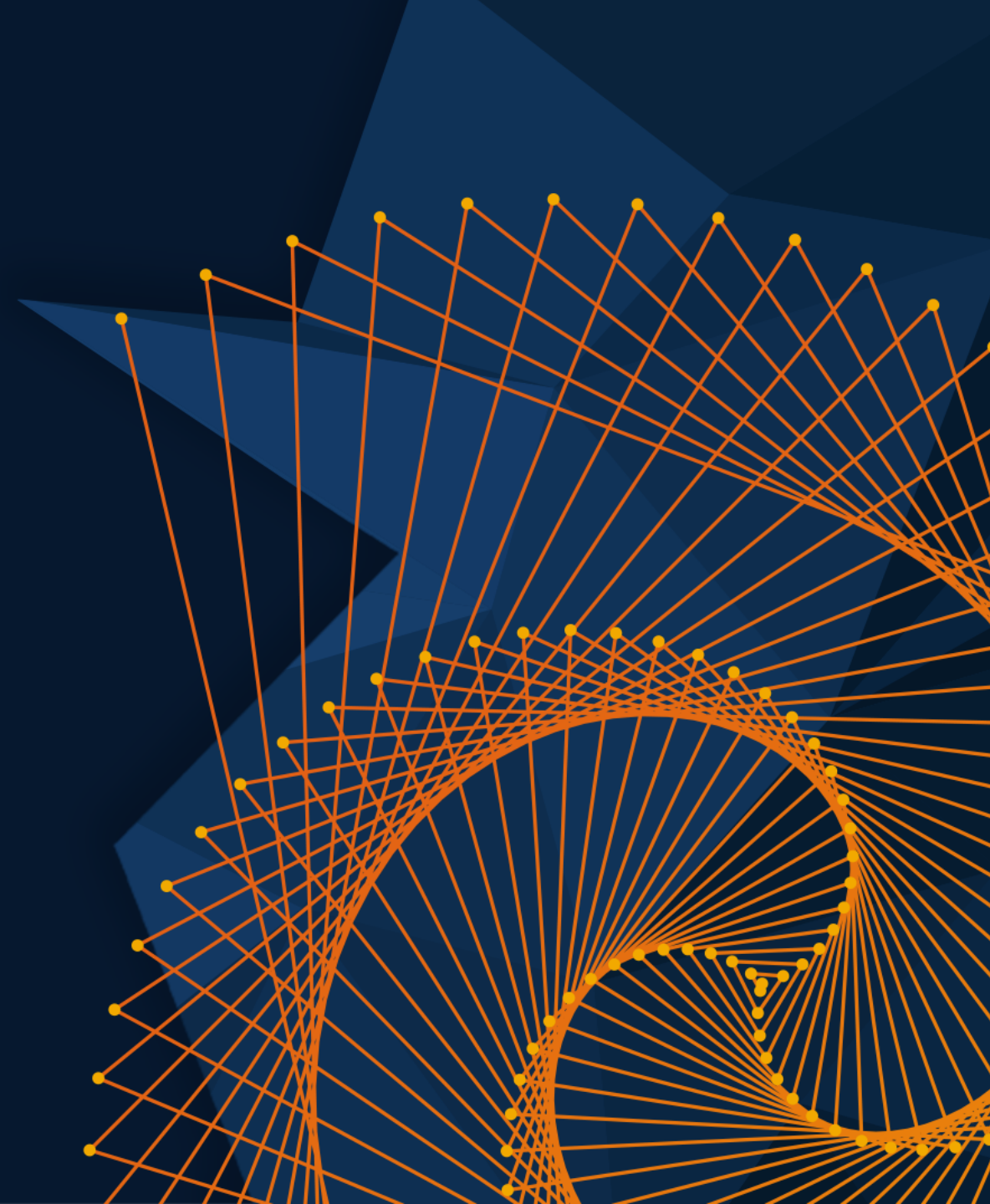
- Control input based on experiment
- except : EXV (SH control)

Simulation (Heating mode around -5°C , cloudy)

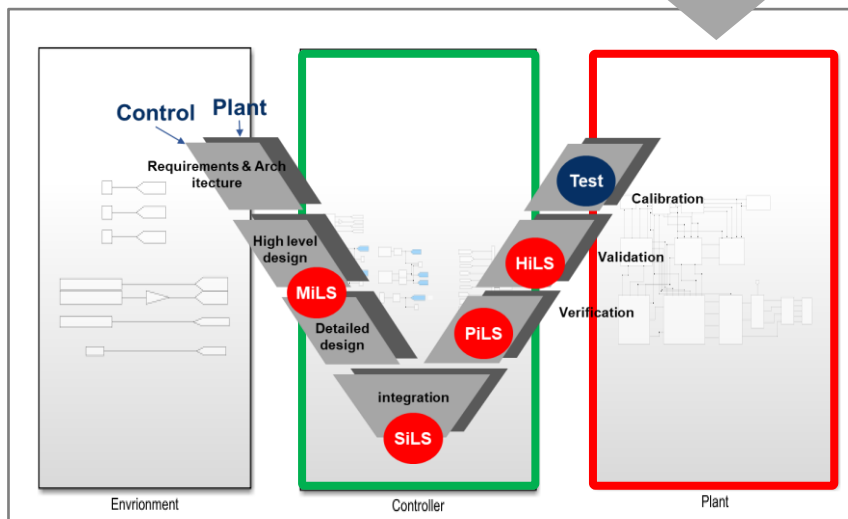
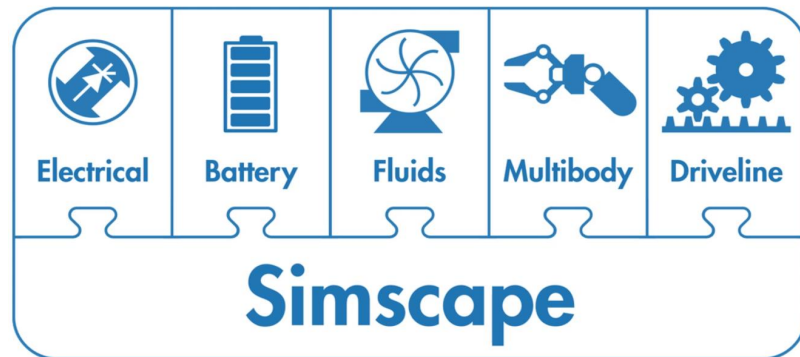


Contents

1. Introduction
2. Component level
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5. Conclusion



1. Component & System level using simscape

- Heat Exchanger : TL-MA, TL-2P, 2P-MA
- Compressor, Cabin
- Integration for thermal circuit & Tube pipe

2. Control logic for simscape

- Discrete signal – Transfer fcn – Continuous signal

3. Virtual Plant (simscape) with controller

- Virtual plant performance → thermal circuit, size decision
- Logic performance → advanced control logic development
- Various physical data